

2023 PSE+ Stakeholder Workshop: Carbon Capture Simulation for Industry Impact (CCSI²)

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CCSI² – Modeling, Optimization, and Technical Risk Reduction



Multi-lab modeling initiative to support carbon capture technology development

















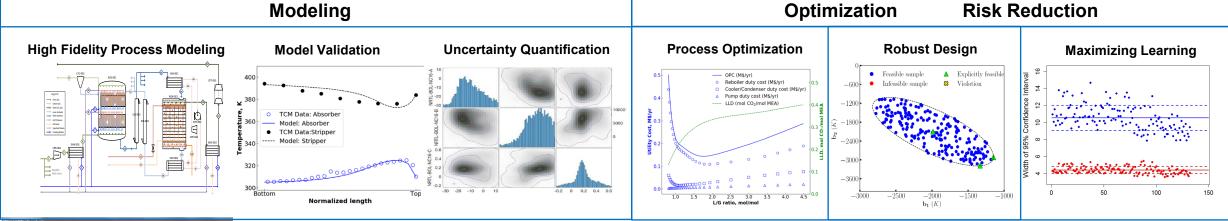














Open Source: github.com/CCSI-Toolset





Past and Present CCSI/CCSI² Industrial Collaborations

























Solids heat exchanger modeling and bottlenecks

Key characterizers of amino-silicone solvent performance

Dynamic CCS modeling and advanced process control (power/steel)

Sorbent pilot test support via DoE

NAS solvent process modeling and pilot support via SDoE Solvent VLE and emissions modeling

EEMPA solvent and process modeling and optimization

Membrane module and process modeling for pilot support

Cryogenic capture process modeling

Membrane module and process modeling (steel)

Piperazine process modeling

Requested to support mixed salt solvent pilot via SDoE

Requested to support sorbent pilot via SDoE

MEA Baseline Campaign process modeling and SDoE

MEA Baseline Campaign process modeling and SDoE

*Highlighted by Marty Lail at 1:30 on Oct 11th

*Poster by Josh Morgan

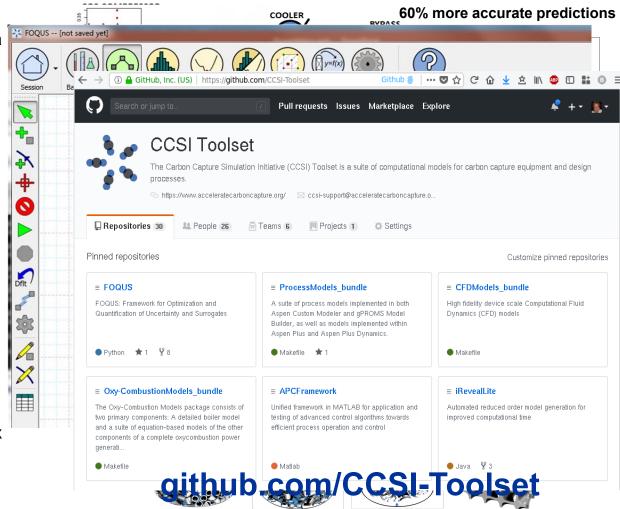
Since 2010 CCSI/CCSI² Supported 16 Carbon Capture projects \$100MM+ in total project value (TRL 3-7)





CCSI² Summary, Capabilities, Highlights

- Sequential Design of Experiments for lab-, bench-, or pilottesting
 - Improves model while optimizing lab- or pilot-scale experimental data generation – can save years off of pilot test schedule
 - NCCC and TCM MEA pilot models accurate on CO₂ Capture percentage within 3-6% with 95% confidence
- Novel Solvent and Process Optimization
 - CFD to elucidate novel solvent/packing interaction, contact angle, interfacial area.
 - Rigorously ensures proper balance of cost and performance.
 Minimize captured cost of 1. PNNL CO₂BOL Process (>10% improvement over baseline), 2. Advanced Solvent Flash Stripper Process (optimization performed for multiple solvents)
- Process Intensification/Equipment Design
 - Intensified solvent absorber design can improve capture rates by >10%
- Machine Learning
 - Increased speed of CFD based hydrodynamic simulations by 4000x for 13-22% accuracy (or 14x with better accuracy)
- Computational Toolset Maintenance
 - Regular software updates and revision management open source





Toolset Publicly Available

*More Detail by Ryan Hughes at 1:15 on Oct 12th



CCSI Toolset

github.com/CCSI-Toolset

The Carbon Capture Simulation Initiative (CCSI) Toolset is a suite of computational models for carbon capture processes.

https://www.acceleratecarboncapture.org/

ccsi-support@acceleratecarboncapture.o...

Repositories 30

A People 26

Teams 6

Projects 1

Settings



Pinned repositories

■ FOQUS

FOQUS: Framework for Optimization and Quantification of Uncertainty and Surrogates

Pytho

★1



■ ProcessModels bundle

A suite of process models implemented in both Aspen Custom Modeler and gPROMS Model Builder, as well as models implemented within Aspen Plus and Aspen Plus Dynamics.

Makefile



≡ CFDModels_bundle

High fidelity device scale Computational Fluid Dynamics (CFD) models

Automated reduced order model generation for

Makefile

≡ iRevealLite

Main website:

https://www.acceleratecarboncapture.org/

Support/Contact Us email:

ccsi-support@acceleratecarboncapture.org

FOQUS User Documentation:

https://fogus.readthedocs.io

YouTube Channel - tutorials:

https://www.youtube.com/channel/UCBVjFnxrs WpNlcnDvh0 GzQ/

FOQUS GitHub repo - development:

https://github.com/CCSI-Toolset/FOQUS

■ Oxy-CombustionModels bundle

The Oxy-Combustion Models package consists of two primary components: A detailed boiler model and a suite of equation-based models of the other components of a complete oxycombustion power generati...

Makefile

■ APCFramework

Unified framework in MATLAB for application and testing of advanced control algorithms towards efficient process operation and control

Matlab

Java

83

improved computational time







































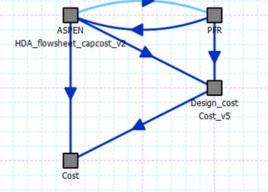


- Interface connecting commercial and open source modeling platforms (Aspen, gPROMS, Python, Pyomo, Excel). Uses your models.

- Propagates uncertainty through modeling hierarchy. Data visualization, parameter screening.

- Simulation based optimization of modeling ensemble.

- Optimization of modeling ensemble incorporating parameter-based uncertainty.



- Sequential Design of Experiments (SDoE) maximize learning from experimentation. Uniform and non-uniform space filling. Ordering.
- *More Detail by Abby Nachtsheim and Alex Dowling at 1:15 on Oct 12th and Poster by Jialu Wang
- Surrogate modeling capabilities to reduce computational burden of simulation-based engineering. Now coupled with optimization.



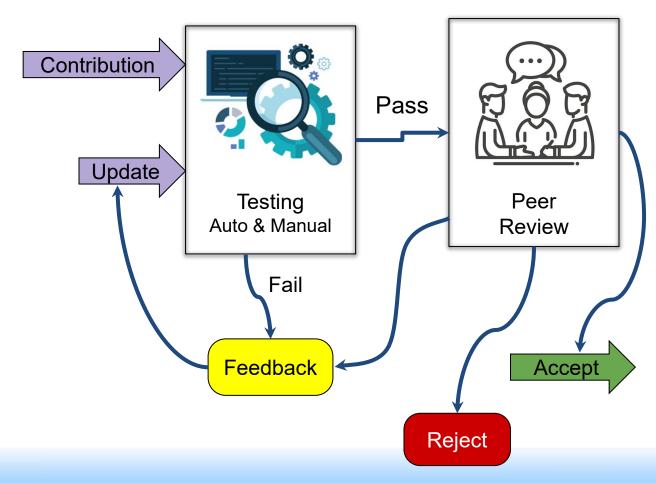
Open Source Toolset Development and Maintenance

- Code publicly available since 2017
- Permissive 3-clause BSD license
- All may use, modify or distribute (with attrib.)
- Examination and contributions welcomed

All Changes Tested and Reviewed

- Currently being used by dev team
- Contributions are tested (manual & auto)
- Peer reviewed by core team members
- Feedback, conversation, changes...
- Change is accepted or rejected
- NDA-Protected IP uses identical process

Two-Stage Code Review Process





SDoE Executive Summary

- First-principles modeling serves as the foundation for pilot campaign designs
- UQ can be used to identify data gaps and their effect on key metrics
- SDoE leverages UQ to more efficiently inform data collection
 - Improves MEA CO₂ capture rate prediction by ~60%
- Improved models support better optimizations
- Optimization under more refined uncertainty leads to more robust designs
- Modeling insights can be used to guide future R&D decisions more efficiently



Deterministic Solvent Modeling Framework

Vapor-Liquid Equilibrium

$$\hat{f}_i^V = \hat{f}_i^L \longrightarrow \hat{\varphi}_i y_i P = \gamma_i^* x_i H_i$$
 (for solutes)

Activity Coefficient

$$ln(\gamma_i) = \frac{1}{RT} \frac{\partial (nG^{ex})}{\partial n_i} \bigg|_{T,P,n_{j \neq i}} \qquad \gamma_i^* = \frac{\gamma_i}{\lim_{x_i \to 0} \gamma_i}$$

Reaction Equilibrium Constant

$$\Delta G_{rxn} = -RTln(K)$$

Enthalpy Equations

Excess Enthalpy

$$H^{ex} = -RT^2 \sum_{i} x_i \left(\frac{\partial \ln \gamma_i}{\partial T} \right) \bigg|_{P,x}$$

Heat Capacity

$$H_m^l(T + \Delta T) - H_m^l(T) = \int_T^{T + \Delta T} C_{p,m}^l dT$$

Heat of Absorption

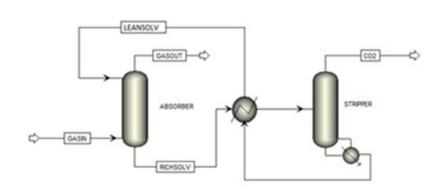
$$\Delta H_{abs} = \frac{n_{final}H_{final} - n_{initial}H_{initial} - n_{CO_2}H_{CO_2}}{n_{CO_2}}$$



Deterministic Solvent Modeling Framework











- Validated for National Carbon Capture Center (NCCC) (MEA solvent)
- Validated for Technology Centre Mongstad (TCM) (MEA solvent)



Solvent Model Validation Hierarchy

Rationale

- Fundamental interactions between CO₂ solvent and absorber packing are poorly propagated between material and process length scales.
- Absorber packing sizing and performance predictions are largely empirically based, and often use low fidelity engineering safety factors to account for unknown commercial scale uncertainties.

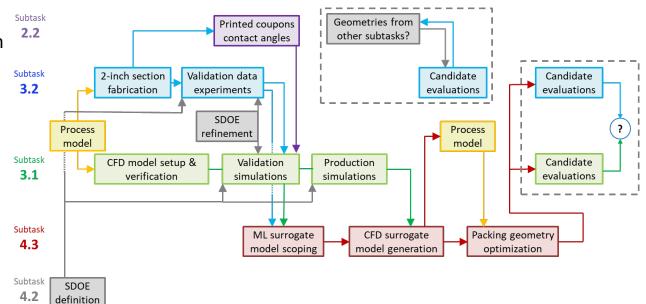
Approach

- Develop fundamental models of governing phenomena at each length scale
- Couple multi-scale and multi-physics models, reduce model complexity while retaining sufficient accuracy for meaningful performance predictions
- Validate models by generating prototype packing and testing carbon capture performance across a range of conditions, including arbitrary heat management throughout the column length.

Outcome

- A **cohesive modeling framework** that can propagate behavior induced by solvent, packing geometry, and packing material choices from the droplet scale through the process scale.
- Fundamental understanding of how to optimize absorber design/operation for arbitrary solvents and capture targets.

Solvent Model Validation Hierarchy Workflow











Solvent Contact Angle

8" column

12" column

3D printed intercooled packing



Novel Solvent-Specific Uncertainty Quantification

Activity Coefficients

$$\ln \gamma_i \ = \frac{\sum_{j} X_j G_{j,i} \tau_{j,i}}{\sum_{k} X_k G_{k,i}} + \sum_{j} \frac{G_{i,j} X_j}{\sum_{k} G_{k,j} X_k} \cdot \left(\tau_{i,j} - \frac{\sum_{m} X_m G_{m,j} \tau_{m,j}}{\sum_{k} X_k G_{k,j}} \right)$$

$$\ln H_{ia} = A_{ia} + \frac{B_{ia}}{T}$$

$$\tau_{i,j} = A_{i,j} + \frac{B_{i,j}}{T}$$

$$\ln P_i^{vap} = A_i + \frac{B_i}{T + C_i}$$

$$G_{i,j} = e^{\left(-\alpha_{i,j}\tau_{i,j}\right)}$$

Mass Transfer

$$k_G = D_G C_G \left(\frac{a}{d_H}\right)^{0.5} S c_G^{0.333} R e_G^{0.75} \sqrt{\frac{1}{\varepsilon - h_L}}$$

Viscosity

$$\ln \mu_{BOLs} = A_{BOLs} + \frac{B_{BOLs}}{T} + C_{BOLs} \cdot \ln T$$

$$w_{H2O} = \frac{\alpha_{H2O} \cdot MW_{H2O}}{\alpha_{H2O} \cdot MW_{H2O} + MW_{BOL}}$$

$$\mu_{BOLs-H2O} = \mu_{BOLs} \cdot (1 - w_{H2O}) + \mu_{H2O} \cdot w_{H2O} + D_{Binary} \cdot w_{H2O} \cdot (1 - w_{H2O})$$

$$\mu_{BOLs-CO2-H2O} = \mu_{BOLs-H2O} \cdot e^{\alpha_{Co2} \cdot E_{CO2}}$$

Kinetics

$$2CO_2 + 2BOL \leftrightarrow \{BOL - CD^+\} + \{BOL - CD^-\}$$

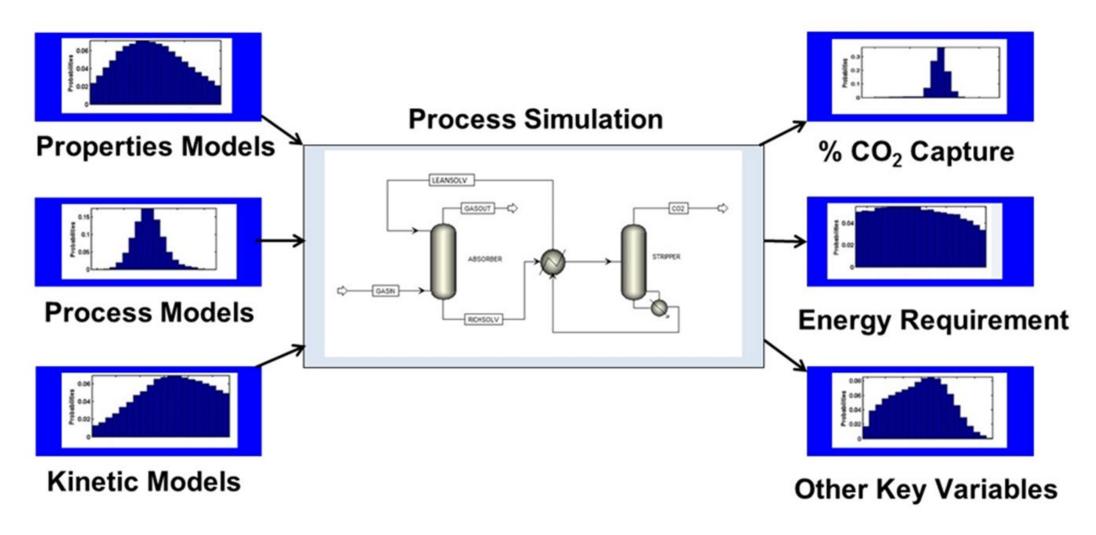
$$r_1 = k_1 \exp\left(-\frac{E_1}{R} \left(\frac{1}{T} - \frac{1}{T^{ref}}\right)\right) a_{CO_2} a_{BOL} \left(1 - \frac{a_{BOL - CD^+} a_{BOL - CD^-}}{(a_{CO_2} a_{BOL})^2 K_1}\right)$$

$$CO_2 + BOL + H_2O \leftrightarrow \{BOLH^+\} + \{HCO_3^-\}$$

$$r_2 = k_2 \exp\left(-\frac{E_2}{R} \left(\frac{1}{T} - \frac{1}{T^{ref}}\right)\right) a_{CO_2} a_{BOL} a_{H_2O} \left(1 - \frac{a_{BOLH} + a_{HCO_3^-}}{K_2}\right)$$



Novel Solvent-Specific Uncertainty Quantification





Bayesian Inference

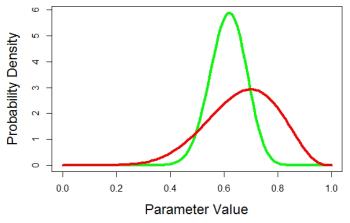
 <u>Bayesian Inference</u> provides a framework for updating beliefs of model parameters characterized by epistemic uncertainty in light of collection of new data

$$\pi(\theta|Z) \propto P(\theta) * L(Z|\theta)$$
Posterior Prior Likelihood

Typical likelihood function (represents discrepancy between model predictions and data values of the output:

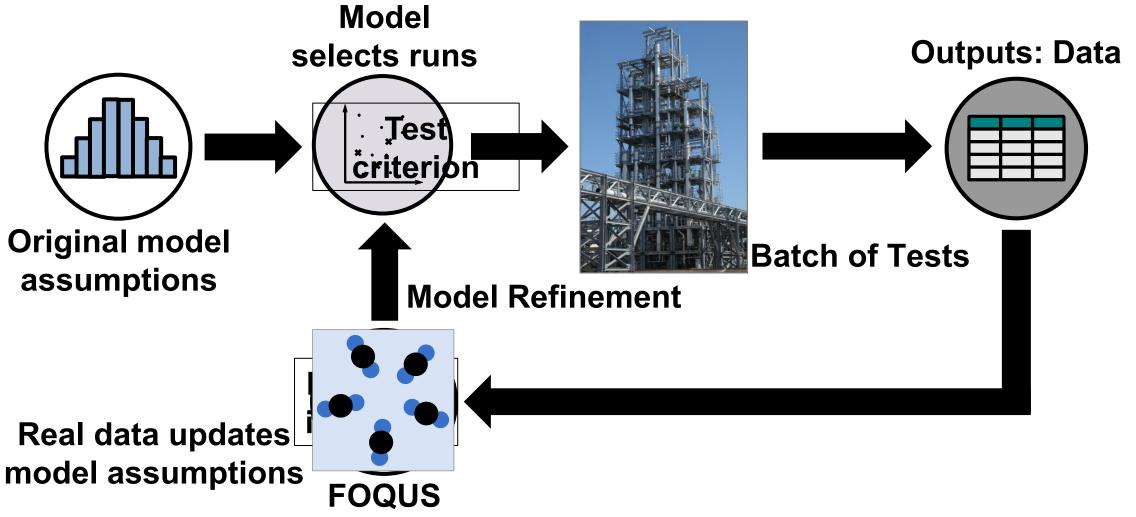
$$L(Z|\theta) = exp\left(-0.5\sum_{i=1}^{M} \frac{\left[F^*(x_i,\theta) - Z(x_i)\right]^2}{M\sigma_i^2}\right)$$

Representation of Prior and Posterior Distributions (reduction in uncertainty through data collection):



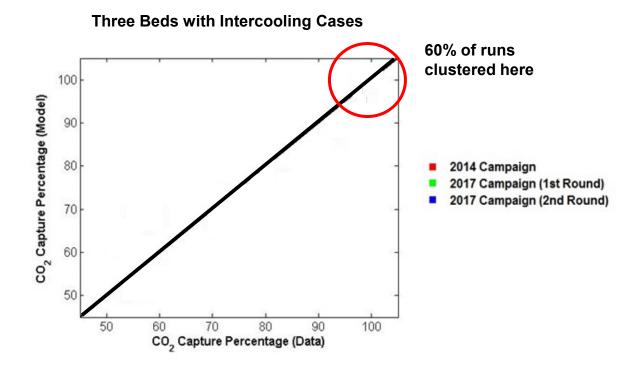


Sequential Design of Experiments Leverages Real Time Data Generation for Optimal Batch Generation



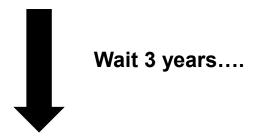


NCCC Model Improvement with SDoE Implementation



2014 Campaign (Before SDoE)

- Conventional test plan caused "clustering"
- Not ideal for complete understanding
- Used data to refine model



2017 Campaign (Using SDoE)

- Much more distributed output
- Much more complete understanding
- *In manner of weeks*, further reduced uncertainty in capture rate by 60%

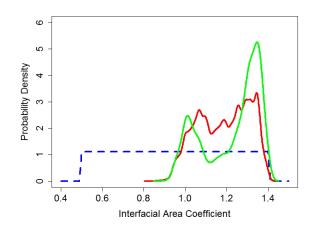


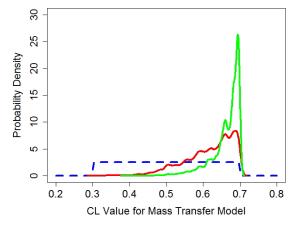
TCM Model Improvement with SDoE Implementation

Update in Parameter Distributions for Absorber Packing



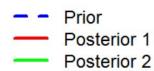
Reduction in CO₂ Capture Percentage Prediction Accuracy

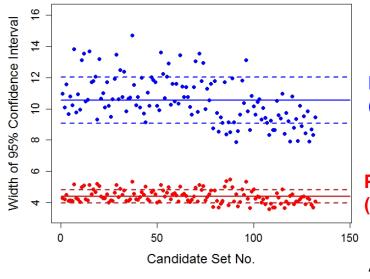




Mass transfer and interfacial area parameters are packing-dependent, and therefore are assigned uniform prior distributions over wide ranges, indicating assumption of relatively large uncertainty before collection of process data.

Bayesian inference, through process data collected using SDoE, results in refined estimates of parameters, and thus reduction in uncertainty in process model and risk associated with scale-up





Prior CI Width: (10.5 ± 1.5)%

Posterior CI Width: (4.4 ± 0.4)%

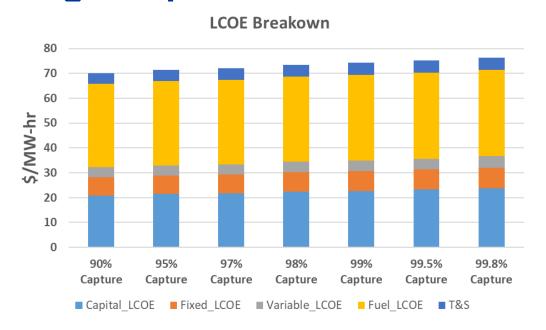
Average reduction in uncertainty: 58.0 ± 4.7%

Candidate set includes variation in:

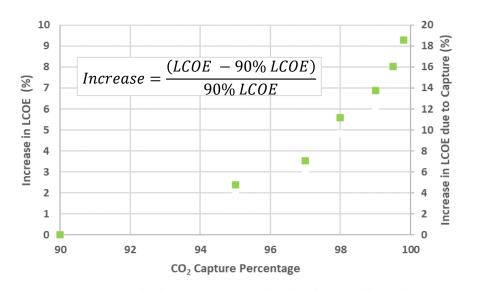
- Solvent Circulation Rate
- Flue Gas flowrate and CO₂ concentration
- Reboiler steam flowrate

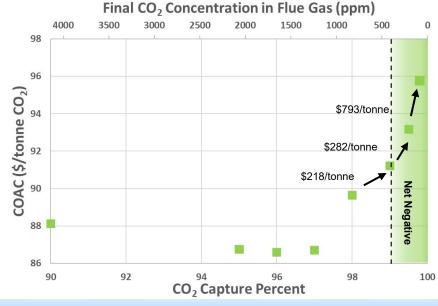


High Capture Rates with MEA Solvent - NGCC



- LCOE increases linearly from 90→98%, relatively constant cost of avoided CO₂.
- Incremental cost of avoided CO₂ significantly increases in 98→99.8% capture range.
- Practical considerations (e.g., need for aux boiler, flexible operation) will increase LCOE further at high capture percentages

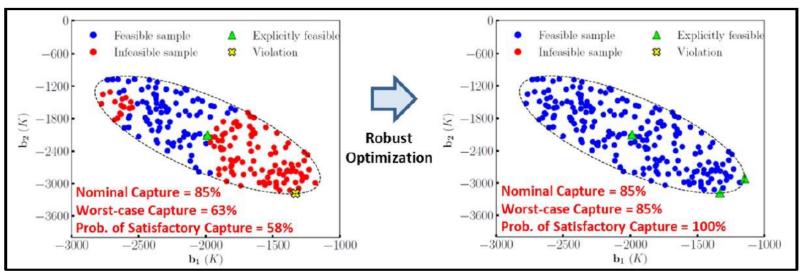








PyROS: a Pyomo Robust Optimization Solver

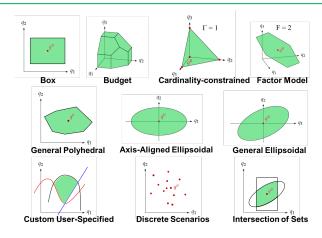


Designs optimized deterministically <u>can easily</u> <u>become infeasible</u> with moderate uncertainty

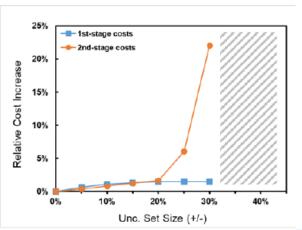
Robust optimized designs can ensure safety and performance constraints are met amidst anticipated uncertainty

Price of robustness can be quantified, minimized

*More Detail in Poster by Jason Sherman



Evolution of costs for increasingly robust designs





Capture Modeling and Analysis Capabilities

Tools and process models to predict, optimize, and minimize risk in the scale-up of technologies



*Posters by: Morgan, Panagakos, Xu. Summits. Tsouris

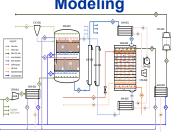
*Posters by: Morgan, Hughes, Hedrick

*Demo by: Hughes, Hedrick





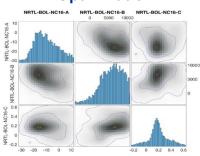




Process-level TEA



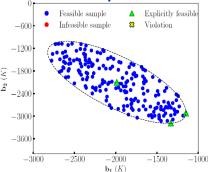
UQ and Parameter **Optimization**



Foundational Capabilities

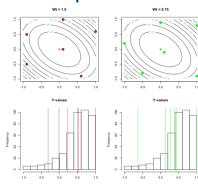
- High-Fidelity CCS Modeling (sorbents, solvents, membranes)
- **Design of Experiments**
- Steady-State and Dynamic Process Optimization
- Electricity Grid Modeling / Expansion Planning
- Multi-Scale Modeling and Optimization (Materials/Process/Grid)
- **Uncertainty Quantification**
- Robust Optimization (i.e., Design Under Uncertainty)
- Machine Learning/Al

Robust Optimization



*Poster by: Sherman

Optimal DoE



*Posters by: Nachtsheim, Wang



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🧡 WestVirginiaUniversity | **West Virginia University**: Debangsu Bhattacharyya, Stephen Summits



University of Notre Dame: Alexander Dowling, Jialu Wang



University of Pittsburgh: Katherine Hornbostel

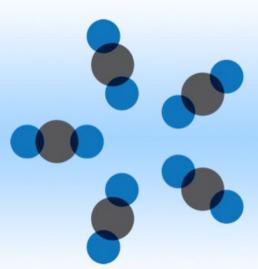


University of Toledo: Glenn Lipscomb



University of Texas at Austin: Gary Rochelle, Miguel Abreu, Ben Drewry, Athreya Suresh, Miguel Torres





Carbon Capture Simulation for Industry Impact

For more information

https://www.acceleratecarboncapture.org/

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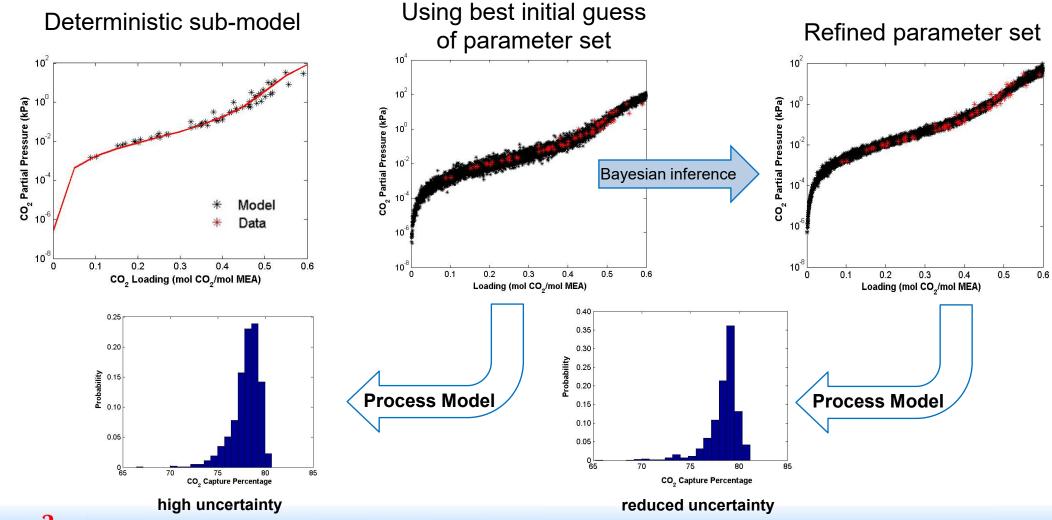






Uncertainty Quantification Bayesian Inference Example: VLE Models

VLE Data/Model Comparison at 40°C

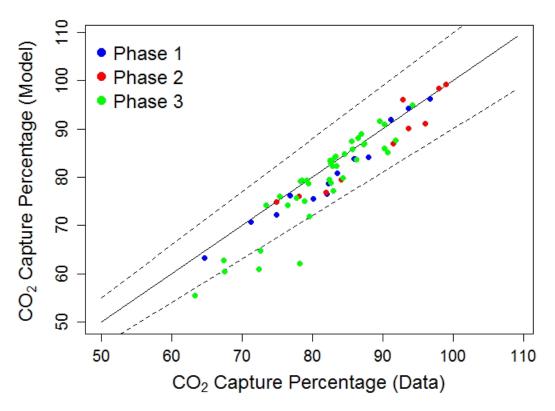


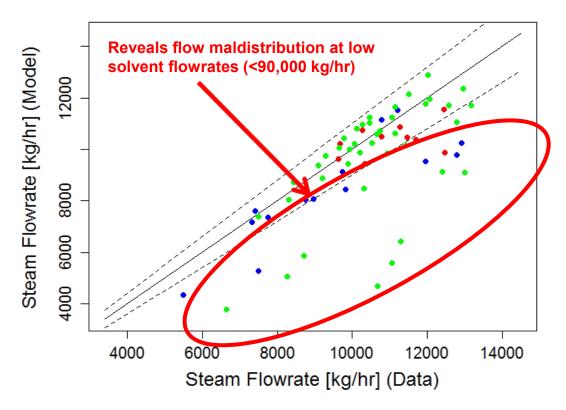


Model Based Insight into Operational Non-Idealities

TCM Absorber Performance*

TCM Stripper Performance*





Fundamental Model Insight into Data Aberrations

