

## Background

- Amine-based CO<sub>2</sub> absorption systems are considered important for CO<sub>2</sub> emissions reduction pathways
- Models for amine-based absorption are highly sensitive to epistemic uncertainty in their thermodynamic and physical property submodels

## Objectives

- Development of a rate-based optimization model for an MEA-based absorption column for CO<sub>2</sub> removal from NGCC flue gas
- Uncertainty quantification (UQ) studies to assess the robustness of deterministically optimal designs
- Two-stage robust optimization (RO) with the recently developed PyROS solver for technical risk reduction

## Absorption Column Model

### Degrees of Freedom:

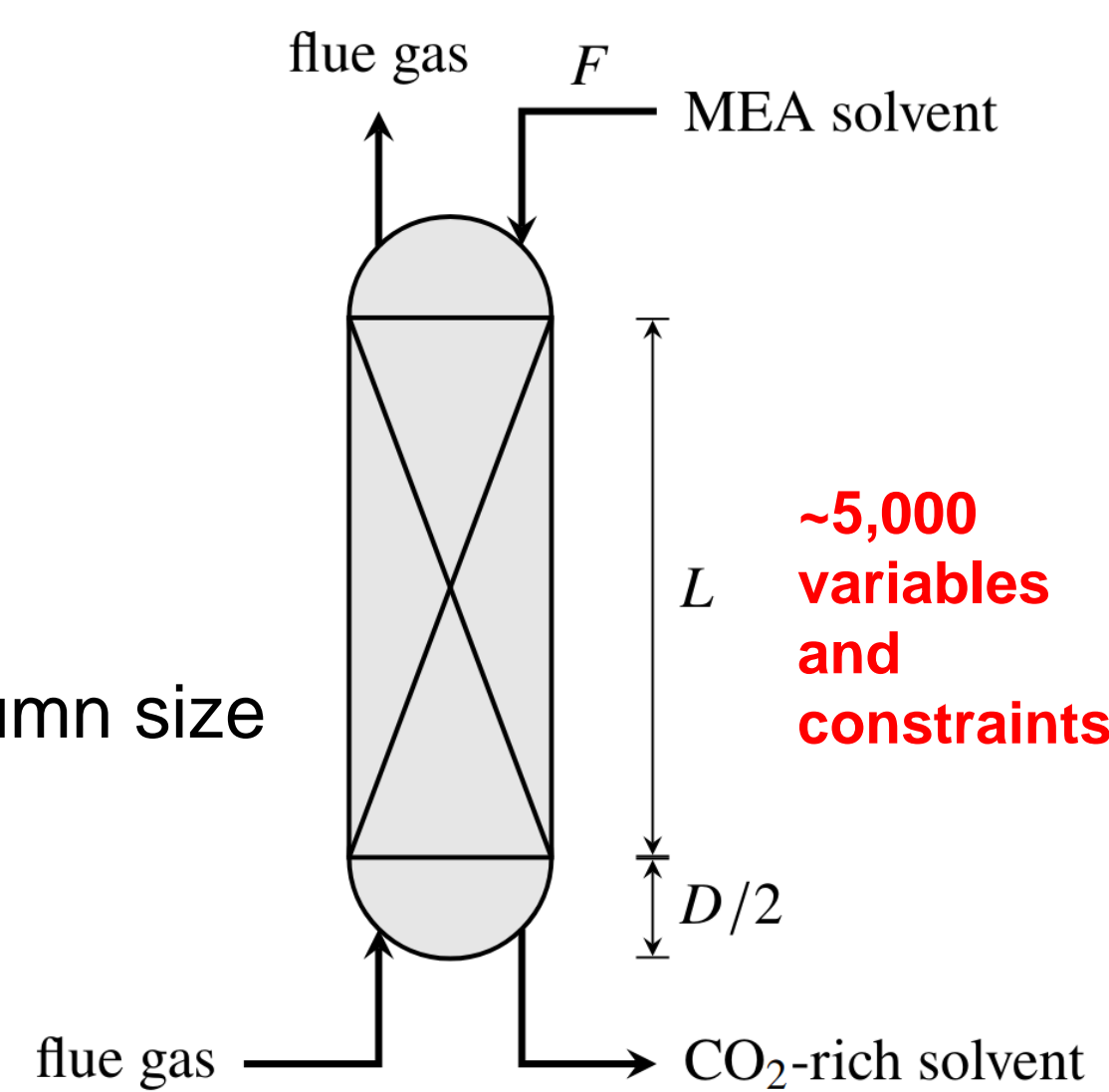
- Column length (L)
- Column diameter (D)
- Solvent recirculation rate (F)
  - adjustable during operation

### Minimize:

- Proxy cost objective combining column size (CAPEX) and MEA flowrate (OPEX)

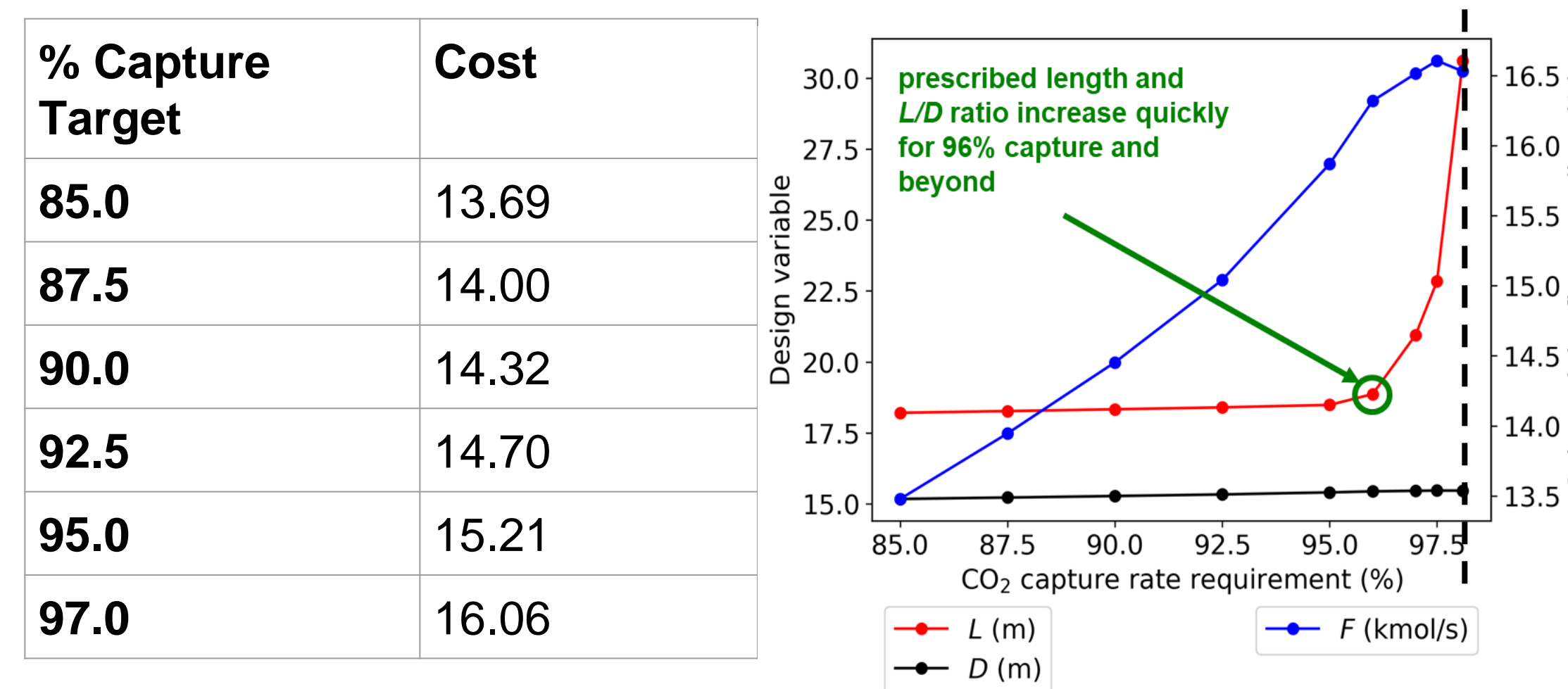
### Subject to:

- Process equality constraints
  - thermodynamic and transport equations
- Sizing constraints
  - bounds on the L/D ratio (1.2–30 used)
- Performance constraints
  - CO<sub>2</sub> capture rate requirement
  - Flooding fraction bound constraints (simplified after rigorous analysis)



## Deterministic Optimization

- Gives **minimal cost designs** for different capture targets
- Model predicts maximum possible CO<sub>2</sub> capture rate of 98.2% (dashed line), we were able to obtain designs for targets up to 98.1%

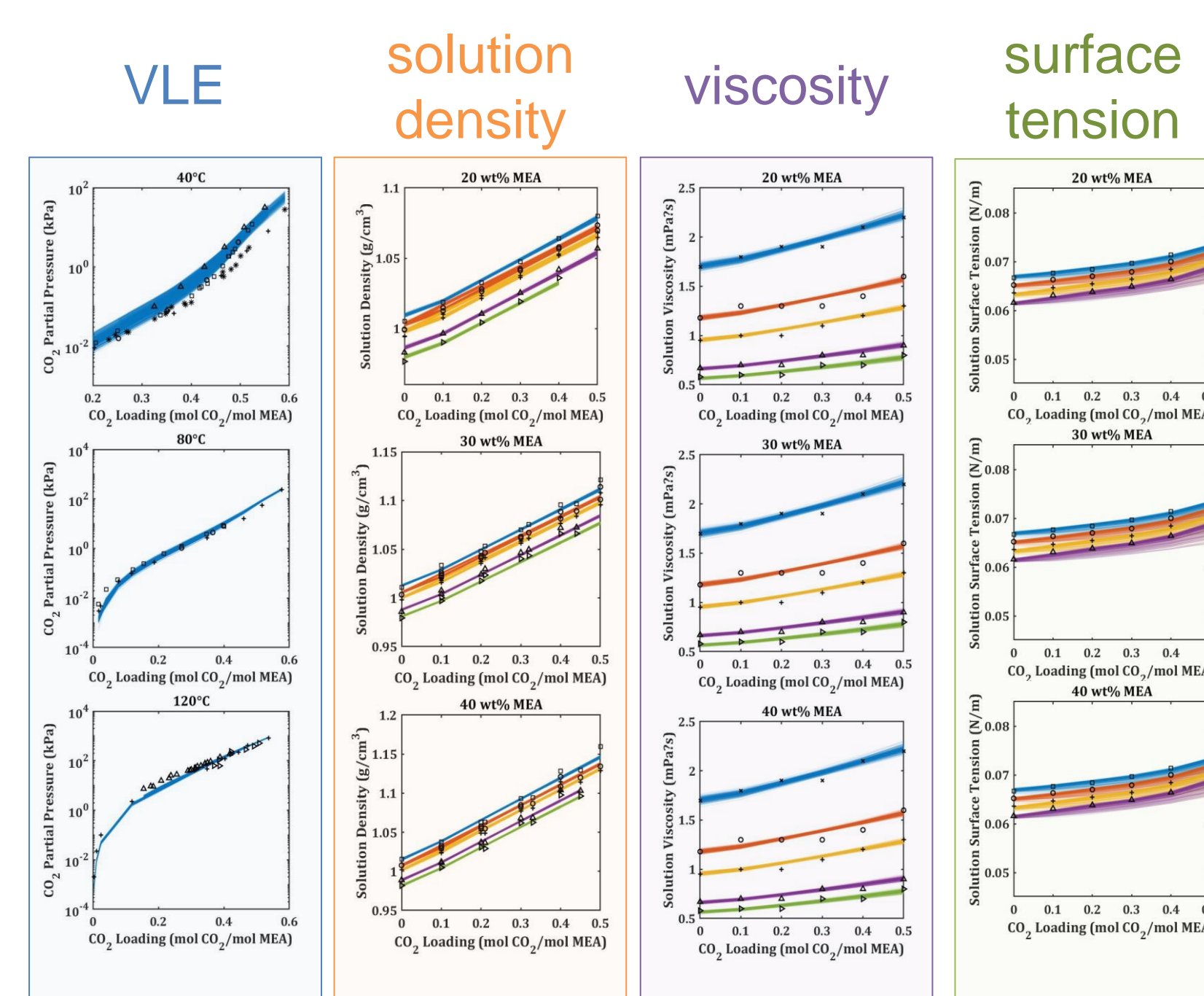


## Non-Robustness of Nominal Designs

- Nominal designs are non-robust and **less likely to adapt to increased capture targets**
- A **significant level of over-design** required to establish guarantees

Deterministic Solution for Min. % CO <sub>2</sub> Capture	Objective (10 <sup>3</sup> m <sup>3</sup> )	Total % Gaussian Probability Mass (and number of realizations out of 200) Feasible Subject to Capture Rate % Requirement of					
		85.0	87.5	90.0	92.5	95.0	97.0
85.0	13.69	48.1 (81)	1.2 (8)	0.0 (0)	0.0 (0)	0.0 (0)	0.0 (0)
87.5	14.00	90.3 (143)	46.9 (75)	3.9 (10)	0.0 (0)	0.0 (0)	0.0 (0)
90.0	14.32	98.5 (180)	81.1 (136)	48.1 (83)	6.0 (23)	0.0 (0)	0.0 (0)
92.5	14.70	99.3 (189)	97.6 (170)	80.8 (132)	48.5 (87)	6.4 (26)	0.1 (3)
95.0	15.21	99.8 (190)	99.3 (186)	97.5 (166)	81.9 (132)	48.2 (82)	11.9 (45)
97.0	16.06	99.6 (189)	99.5 (185)	99.5 (184)	98.2 (172)	81.5 (127)	48.2 (82)

## Parameter Estimation and UQ



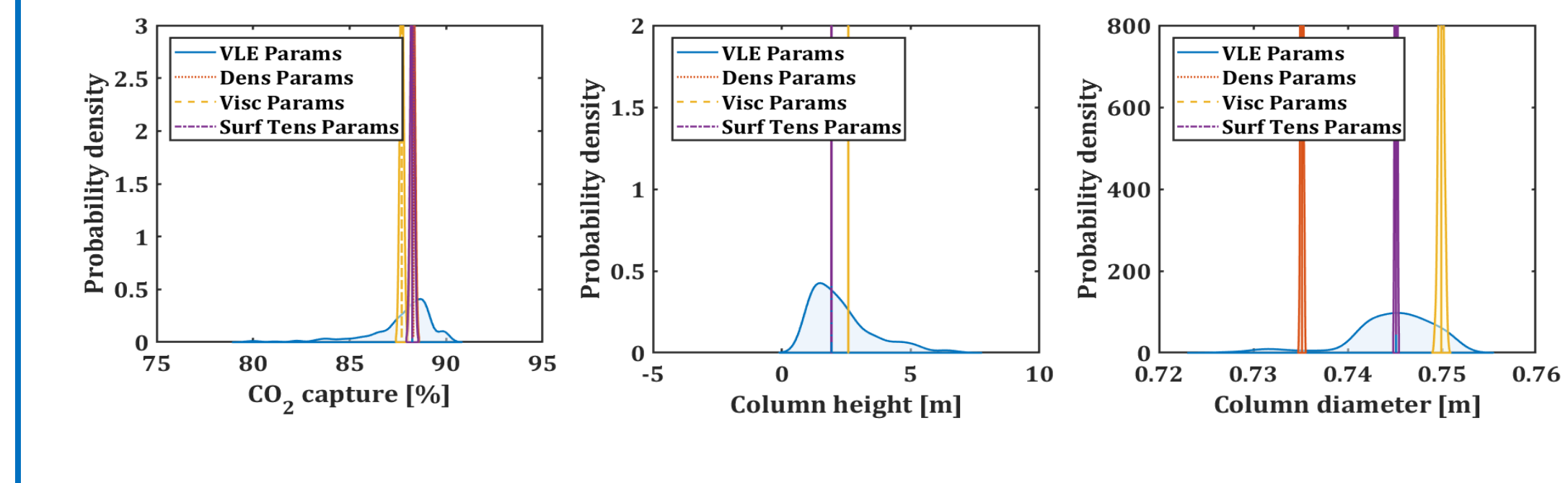
Used **parmesit<sup>1</sup>** to identify point estimates and covariances in:

- vapor-liquid equilibrium (VLE),
- solution density,
- viscosity, and
- surface tension parameters.

### Outcomes:

- (1) Model predictions most affected by uncertainty in VLE parameters
- (2) Insignificant response to uncertainty in the remaining property model parameters

## Uncertainty Propagation through absorption column model:



## Two-Stage Robust Optimization with the PyROS Solver

- PyROS<sup>[2, 3]</sup>: a nonconvex two-stage RO solver based on the Pyomo modeling language. Documentation at: [https://pyomo.readthedocs.io/en/stable/contributed\\_packages/pyros.html](https://pyomo.readthedocs.io/en/stable/contributed_packages/pyros.html)
- Robust designs are **more expensive** than their deterministic counterparts
- Cost increases **only as necessary for increased feasibility guarantees** (more scenarios factored in)
- Such robust design hierarchies establish an upper limit on the **\$ worth spending to reduce uncertainty**
  - e.g., *shall we do more "science" to improve our property models?*

Minimum Capture Rate (%)	Robust Column Proxy Cost and DOF (L, D, F) Values [m, m, kmol/s] for different Confidence Levels			
	0% (deterministic)	90%	95%	99%
90.0	14.32 (18.33, 15.28, 14.45)	17.19 (25.09, 15.51, 17.08)	17.57 (26.43, 15.52, 17.29)	18.37 (29.24, 15.55, 17.76)
92.5	14.70 (18.40, 15.33, 15.04)	18.05 (27.94, 15.54, 17.62)	18.48 (29.50, 15.56, 17.85)	19.40 (32.81, 15.59, 18.33)
95.0	15.21 (18.49, 15.41, 15.87)	19.37 (33.17, 15.58, 18.17)	19.92 (35.33, 15.60, 18.40)	21.14 (40.22, 15.63, 18.87)

## References

- [1] Klise, Nicholson, Staid, Woodruff. *Computer Aided Chemical Engineering*, 47 (2019): 41-46.
- [2] Isenberg, Natalie M., et al. "A generalized cutting-set approach for nonlinear robust optimization in process systems engineering." *AIChE Journal* 67.5 (2021): e17175.
- [3] N.M. Isenberg, J. Sherman, J.D. Sirola, C.E. Gounaris, "PyROS: Nonlinear Robust Optimization in Pyomo," Forthcoming, 2023.

## Acknowledgements

The authors graciously acknowledge funding from the U.S. Department of Energy, Office of Fossil Energy and Carbon Management, through the Carbon Capture Program and Simulation-based Engineering/Crosscutting Research Program. JS and CEG also graciously acknowledge funding from the Carbon Capture Simulation for Industry Impact (CCSI<sup>2</sup>) program.

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