



# 2024 PSE+ Stakeholder Workshop: Carbon Capture Simulation for Industry Impact (CCSI<sup>2</sup>)

**Michael Matuszewski**  
**CCSI<sup>2</sup> Associate Technical Director**

**Pittsburgh Marriott City Center**  
**Pittsburgh, PA**  
**9/18/2024**



U.S. DEPARTMENT OF  
**ENERGY**



Lawrence Livermore  
National Laboratory



West Virginia University



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Carnegie Mellon

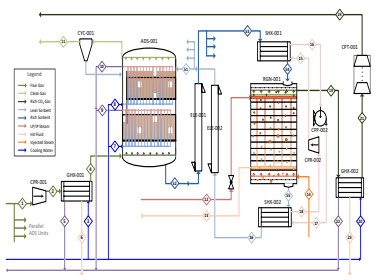
# CCSI<sup>2</sup> – CCS Modeling, Optimization, and Technical Risk Reduction

Multi-lab modeling initiative to support carbon capture technology development

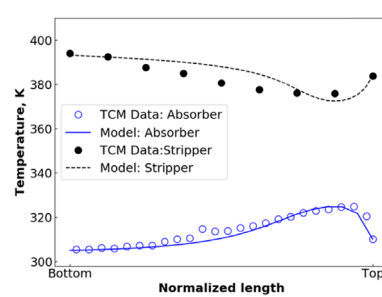


## Modeling

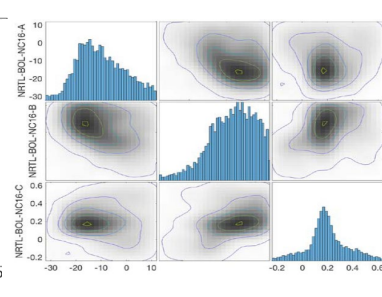
### High Fidelity Process Modeling



### Model Validation

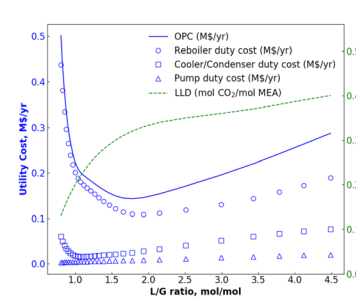


### Uncertainty Quantification



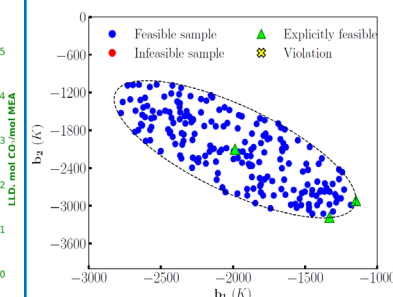
## Optimization

### Process Optimization

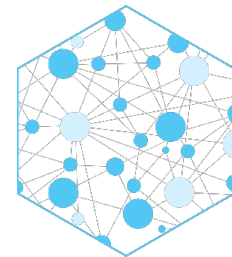
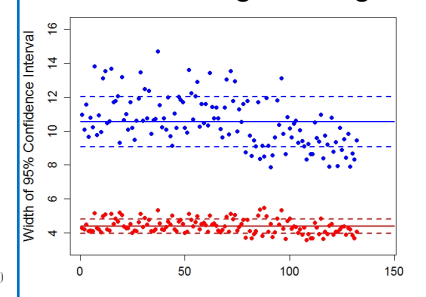


## Risk Reduction

### Robust Design



### Maximizing Learning

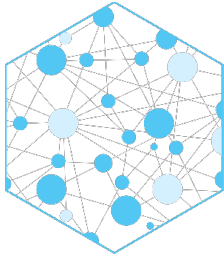


# IDAES

Institute for the Design of Advanced Energy Systems



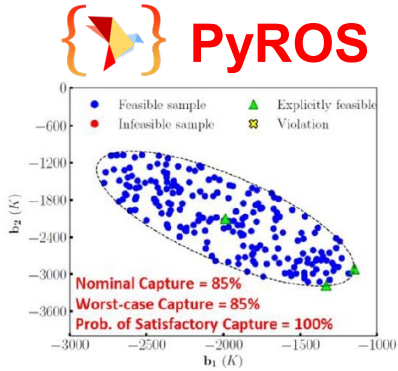
# CCSI<sup>2</sup> Applies IDAES Toolset



## IDAES

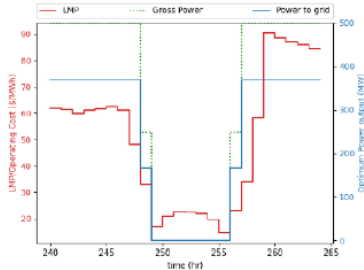
Institute for the Design of Advanced Energy Systems

\*Burgard Wed at 9:15



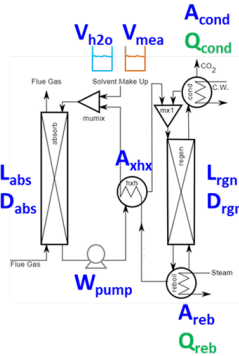
**Robust Optimization**

\*Chrysanthos Thu at 2:30



**Multi-period Optimization**

\*Radhakrishna Thu at 9:30



**MEA Process Model**

\*Poster by Doug Allan



# Mission: Ensure Maximum Value to Tech Developer Pilots

- **First principles based process models** are a key component in demonstrating **risk reduction** for process scale-up
- **Model demonstration and validation** at pilot scale is understood to be an **important component** of relevant funding opportunity announcements (FOA)
- **All pilots** in FOA 2614 Round 3 expected to **develop and validate process models** of their technology
  - Models **do not** have to be provided to NETL/FECM, however details of models and submodels, data sets, and validations will be examined
- **CCSI<sup>2</sup> can provide support** for model development, optimal DoE, uncertainty quantification and validation

# Present CCSI<sup>2</sup> Industrial Collaborations

\*Matuszewski Wed at 3:30



Dynamic CCS modeling and advanced process control (power/steel)



NAS solvent process modeling and pilot support via SDoE



Solvent VLE and emissions modeling



EEMPA solvent and process modeling and optimization



Membrane module and process modeling for pilot support



Membrane module and process modeling (steel)



Piperazine process modeling



*Requested* to support mixed salt solvent pilot via SDoE



MEA Baseline Campaign process modeling and SDoE



MEA Baseline Campaign process modeling and SDoE



Facilitated Transport Membrane modeling and SDoE



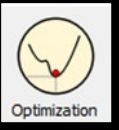

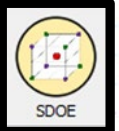



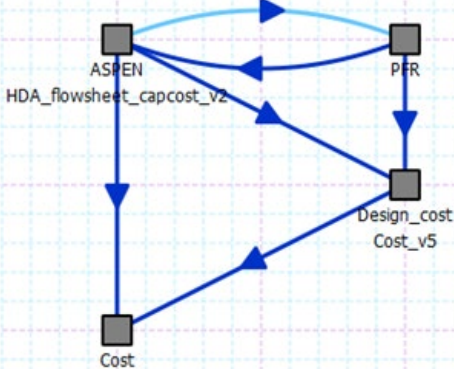
*Requested* to support solvent modeling and SDoE

# How CCSI<sup>2</sup> Adds Value: FOQUS Framework

FOQUS -- [not saved yet]

Session Flowsheet Uncertainty Optimization OUU SDOE Surrogates Settings Help

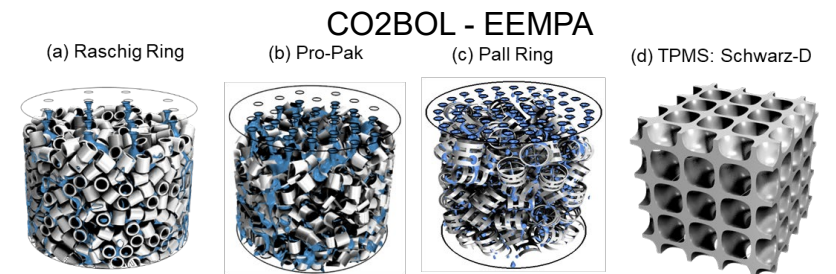
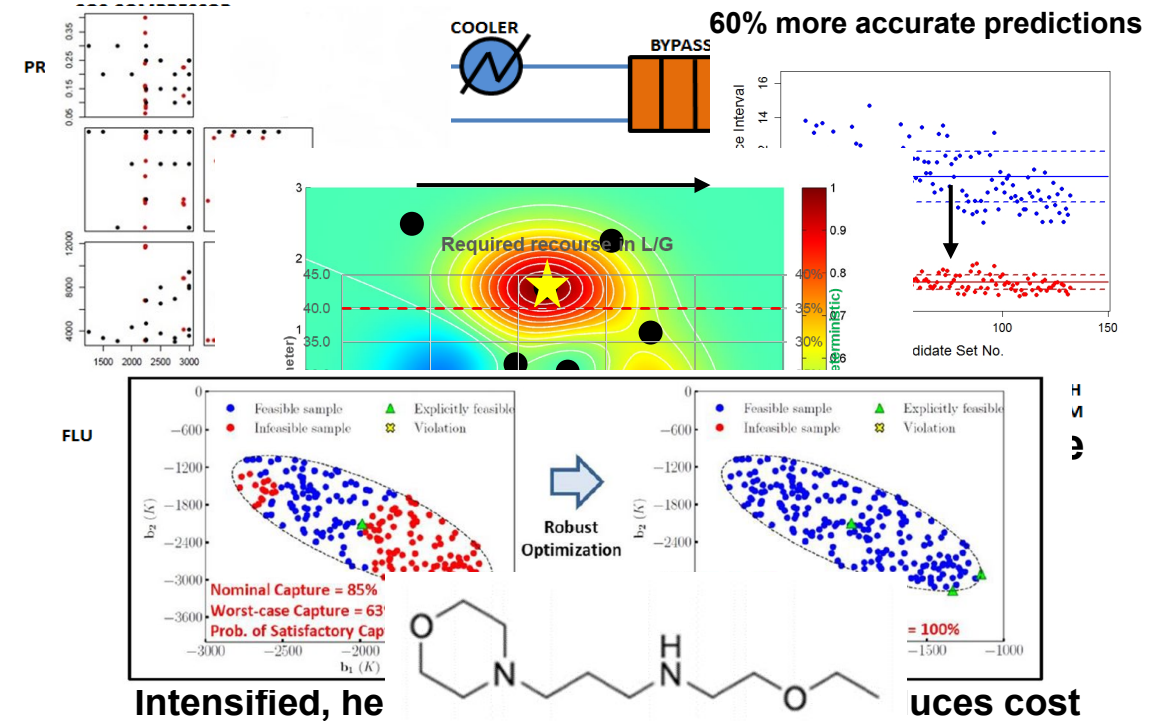
-  - Interface connecting commercial and open source modeling platforms (Aspen, gPROMS, Python, Pyomo, Excel). Uses your models.
-  - Propagates uncertainty through modeling hierarchy. Data visualization, parameter screening.
-  - Simulation based optimization of modeling ensemble.
-  - Optimization of modeling ensemble incorporating parameter-based uncertainty.
-  - Sequential Design of Experiments (SDoE) maximize learning from experimentation. Uniform and non-uniform space filling. Ordering.
-  - Surrogate modeling capabilities to reduce computational burden of simulation-based engineering. Now coupled with optimization.



```
graph TD; ASPEN[ASPEN] --> PFR[PFR]; ASPEN --> Design_cost[Design_cost Cost_v5]; ASPEN --> Cost[Cost]; PFR --> Design_cost; PFR --> ASPEN; Design_cost --> Cost; Cost --> Design_cost;
```

# CCSI<sup>2</sup> Summary, Capabilities, Highlights

- **Sequential Design of Experiments for lab-, bench-, or pilot-testing**
  - Improves model **while** optimizing lab- or pilot-scale experimental data generation – **can save years off of pilot test schedule**
    - NCCC and TCM MEA pilot models accurate on CO<sub>2</sub> Capture percentage within **3-6% with 95% confidence**
- **Uncertainty Quantification**
  - Perspective on whether **fixed process design/operation** is sufficient
  - **Which design variables** are most effective at improving performance
- **Robust Optimization**
  - Optimization **amidst uncertainty** to ensure safe, feasible operation
  - **Cost-optimal over-design**
- **Novel Solvent and Process Optimization**
  - CFD to **optimize contactor geometry**, elucidate novel solvent/packing interaction, contact angle, interfacial areas, etc.
  - Rigorously balances cost and performance, gaining **>10% reduction in captured cost** over designs not using optimization (e.g. EEMPA).
- **Machine Learning**
  - **Increased speed** of CFD based hydrodynamic simulations **by 4000x** for 13-22% accuracy (or 14x with better accuracy)



# CCSI<sup>2</sup> Part of a Family of PSE Projects

*Multi-scale Process  
Modeling and Optimization*

*Uncertainty Quantification  
and Technical Risk Reduction*

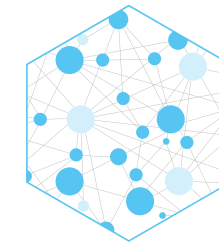
*Design and Operation of  
Dynamic, Interacting Systems*

*Optimization-based Decision  
Support/Operations Research*

## **PSE Application Areas (non-exhaustive):**

- Point Source and Direct Air Capture
- Blue Hydrogen
- Low emission Power Generation
- Solid Oxide Fuel/Electrolyzer Cells
- Supercritical CO<sub>2</sub> Power Cycles
- Integrated Energy Systems
- Rare Earth Element/Critical Mineral Processing
- Water Treatment
- Produced Water Management & Optimization
- Methane Mitigation

**Part of Several Collaborative Efforts Aimed at National and DOE Priorities:**



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Advanced Energy Systems



**PROMMIS**  
Process Optimization and Modeling  
for Minerals Sustainability





# Acknowledgements

The CCSI<sup>2</sup> team gratefully acknowledges support from the U.S. DOE's **Point Source Carbon Capture Program**



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**Lawrence Livermore National Laboratory:** Phan Ngyuen, Brian Bartoldson, Jose Cadena, Amar Saini, Yeping Hu, Pedro Sotorrio, Charles Tong



**Oak Ridge National Laboratory:** Charles Finney, Costas Tsouris, Josh Thompson, Aimee Jackson, Gyoung Jang



**Pacific Northwest National Laboratory:** Jay Xu, Charles Freeman, David Heldebrant, Jie Bao, Yucheng Fu, Richard Zheng, Rajesh Singh



**Los Alamos National Laboratory:** Abby Nachstheim, Jim Gattiker, Sham Bhat, Miranda Martin



**Lawrence Berkeley National Laboratory:** Keith Beattie, John Shinn, Karen Whitenack, Josh Boverhof, Ludovico Bianchi, Sarah Poon



**Carnegie Mellon University:** Chrysanthos Gounaris, Jason Sherman, Grigorios Panagakos



**West Virginia University:** Debangsu Bhattacharyya, Stephen Summits



**University of Notre Dame:** Alexander Dowling, Jialu Wang



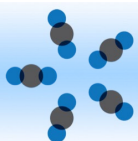
**University of Pittsburgh:** Katherine Hornbostel



**University of Toledo:** Glenn Lipscomb

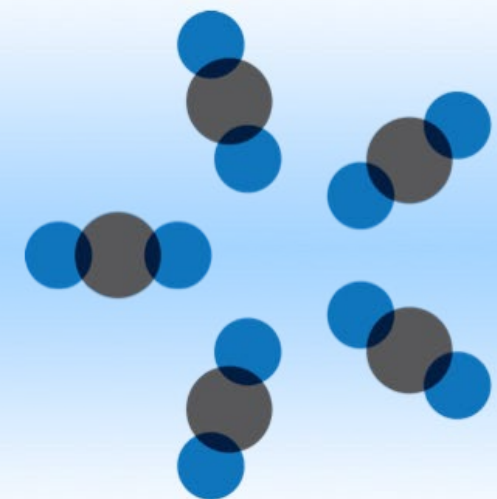


**University of Texas at Austin:** Gary Rochelle, Miguel Abreu, Ben Drewry, Athreya Suresh, Miguel Torres



**CCSI**<sup>2</sup>  
Carbon Capture Simulation for Industry Impact

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# CCSI<sup>2</sup>

Carbon Capture Simulation for Industry Impact

For more information

<https://www.acceleratecarboncapture.org/>

[Michael.matuszewski@netl.doe.gov](mailto:Michael.matuszewski@netl.doe.gov)



2023 Joint CCSI<sup>2</sup>/IDAES Technical Team Meeting, Lawrence Berkeley National Lab



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# Toolset Publicly Available



## CCSI Toolset

The Carbon Capture Simulation Initiative (CCSI) Toolset is a suite of computational models for carbon capture equipment and design processes.

<https://www.acceleratecarboncapture.org/> [ccsi-support@acceleratecarboncapture.o...](mailto:ccsi-support@acceleratecarboncapture.org)

Repositories 30 People 26 Teams 6 Projects 1 Settings

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### FOQUS

FOQUS: Framework for Optimization and Quantification of Uncertainty and Surrogates

Python ★ 1 🍴 8

### ProcessModels\_bundle

A suite of process models implemented in both Aspen Custom Modeler and gPROMS Model Builder, as well as models implemented within Aspen Plus and Aspen Plus Dynamics.

Makefile ★ 1

### CFDModels\_bundle

High fidelity device scale Computational Fluid Dynamics (CFD) models

Makefile

### Oxy-CombustionModels\_bundle

The Oxy-Combustion Models package consists of two primary components: A detailed boiler model and a suite of equation-based models of the other components of a complete oxycombustion power generati...

Makefile

### APCFramework

Unified framework in MATLAB for application and testing of advanced control algorithms towards efficient process operation and control

Matlab

### iRevealLite

Automated reduced order model generation for improved computational time

Java 🍴 3

**Open Source:**  
[github.com/CCSI-Toolset](https://github.com/CCSI-Toolset)  
[github.com/IDAES/idaes-pse](https://github.com/IDAES/idaes-pse)

**Main website:**

<https://www.acceleratecarboncapture.org/>

**Support/Contact Us email:**

[ccsi-support@acceleratecarboncapture.org](mailto:ccsi-support@acceleratecarboncapture.org)

**FOQUS User Documentation:**

<https://foqus.readthedocs.io>

**YouTube Channel - tutorials:**

[https://www.youtube.com/channel/UCBVjFnrxsWpNlcnDvh0\\_GzQ/](https://www.youtube.com/channel/UCBVjFnrxsWpNlcnDvh0_GzQ/)

**FOQUS GitHub repo - development:**

<https://github.com/CCSI-Toolset/FOQUS>

# Capture Modeling and Analysis Capabilities

Tools and process models to predict, optimize, and minimize risk in the scale-up of technologies

\*Posters by: Morgan, Panagakos, Xu, Summits, Tsouris

\*Posters by: Morgan, Hughes, Hedrick

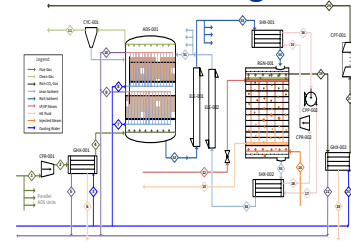
\*Demo by: Hughes, Hedrick

**CCSI<sup>2</sup>**  
Carbon Capture Simulation for Industry Impact

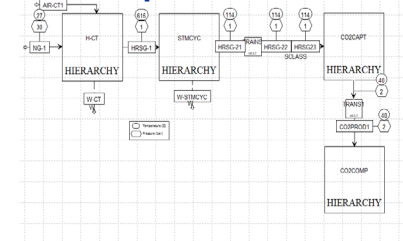
**IDAES**  
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2016 **R&D 100** WINNER

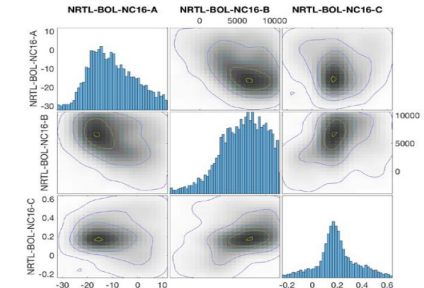
## High-Fidelity, Multi-Scale Modeling



## Process-level TEA Optimization



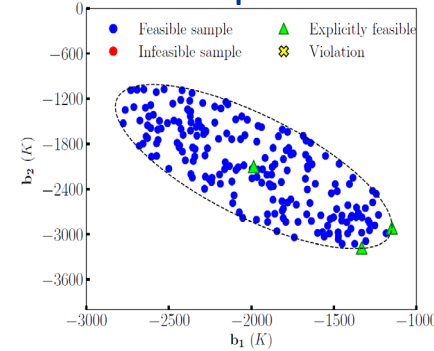
## UQ and Parameter Optimization



## Foundational Capabilities

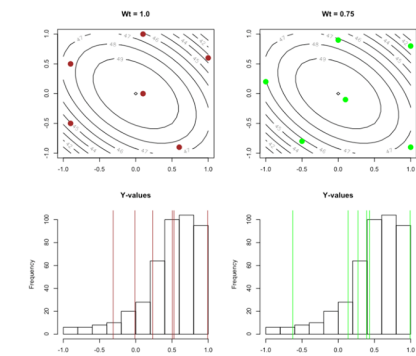
- High-Fidelity CCS Modeling (sorbents, solvents, membranes)
- Design of Experiments
- Steady-State and Dynamic Process Optimization
- Electricity Grid Modeling / Expansion Planning
- Multi-Scale Modeling and Optimization (Materials/Process/Grid)
- Uncertainty Quantification
- Robust Optimization (i.e., Design Under Uncertainty)
- Machine Learning/AI

## Robust Optimization



\*Poster by: Sherman

## Optimal DoE



\*Posters by: Nachtsheim, Wang

**CCSI<sup>2</sup>**  
Carbon Capture Simulation for Industry Impact

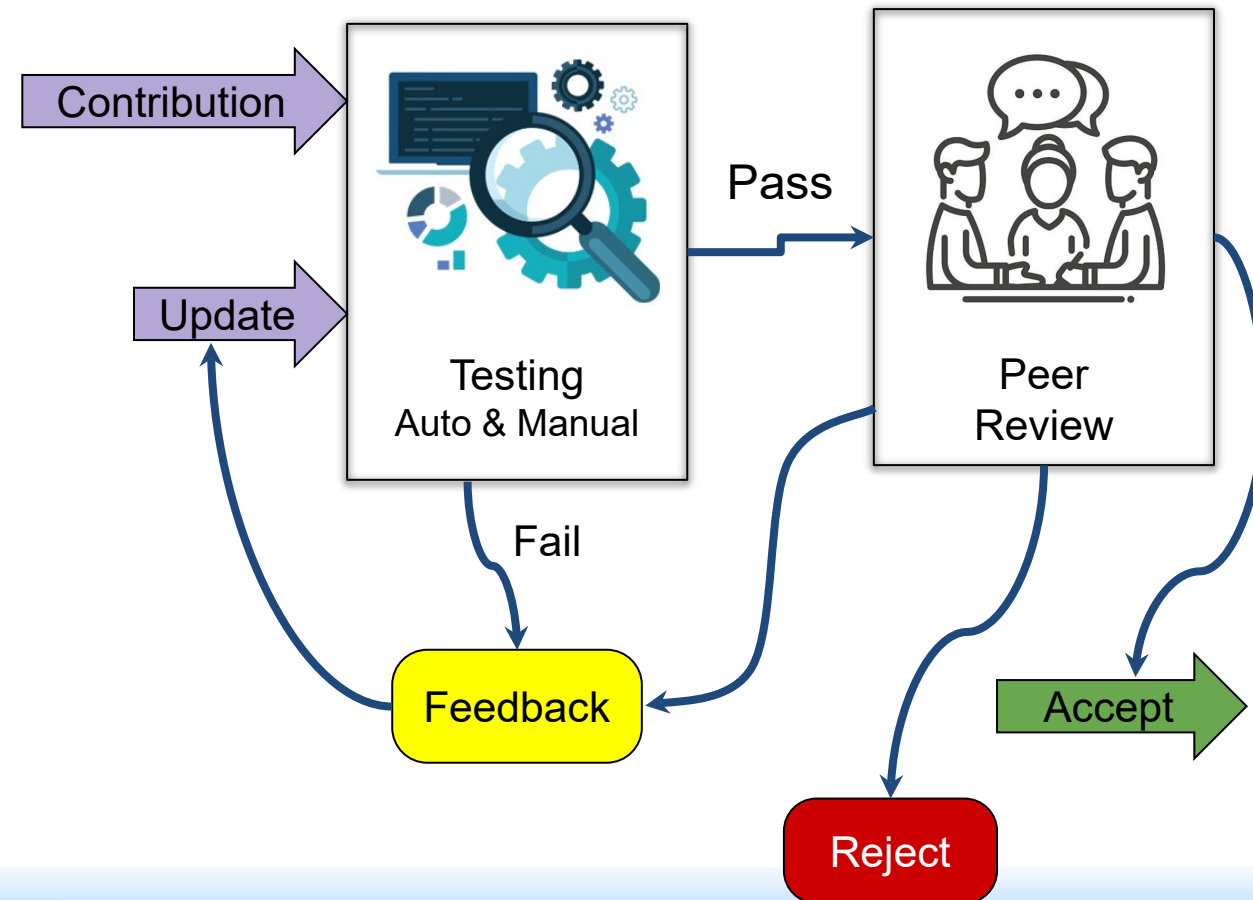
# Open Source Toolset Development and Maintenance

- Code publicly available since 2017
- Permissive 3-clause BSD license
- All may use, modify or distribute (with attrib.)
- Examination and contributions welcomed

## All Changes Tested and Reviewed

- Currently being used by dev team
- Contributions are tested (manual & auto)
- Peer reviewed by core team members
- Feedback, conversation, changes...
- Change is accepted or rejected
- NDA-Protected IP uses identical process

## Two-Stage Code Review Process



# Solvent Model Validation Hierarchy

## Rationale

- **Fundamental interactions between CO<sub>2</sub> solvent and absorber packing** are poorly propagated between material and process length scales.
- Absorber packing sizing and performance predictions are largely empirically based, and **often use low fidelity engineering safety factors** to account for unknown commercial scale uncertainties.

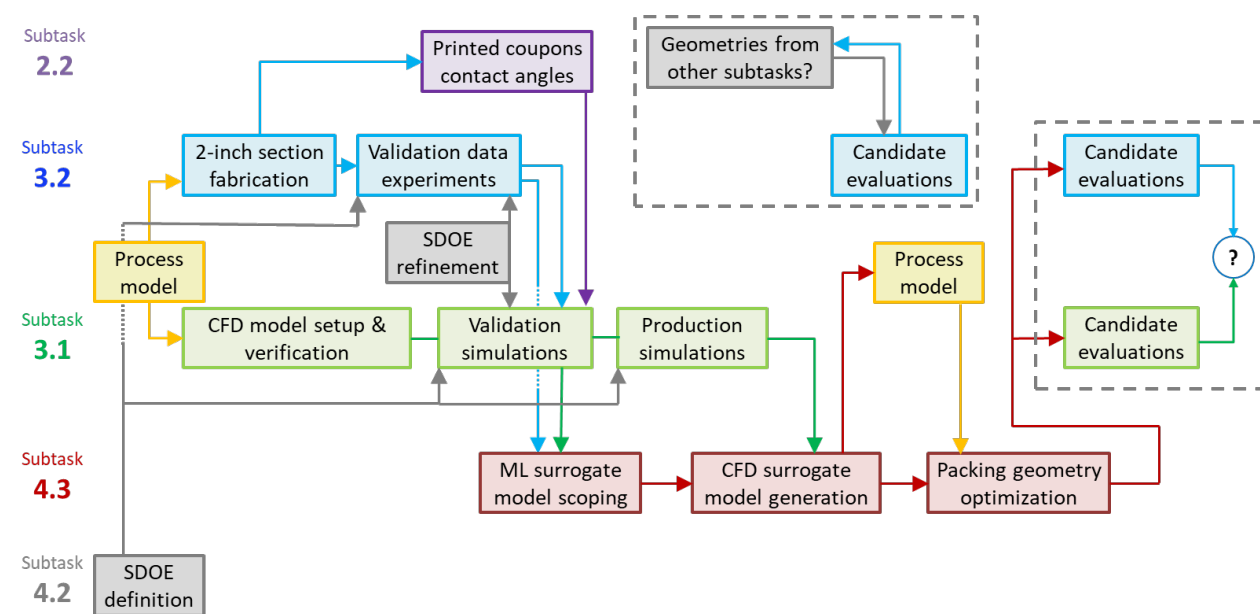
## Approach

- Develop fundamental models of governing phenomena at **each length scale**
- **Couple multi-scale and multi-physics models**, reduce model complexity while retaining sufficient accuracy for meaningful performance predictions
- **Validate models** by generating prototype packing and testing carbon capture performance across a range of conditions, including arbitrary heat management throughout the column length.

## Outcome

- A **cohesive modeling framework** that can propagate behavior induced by solvent, packing geometry, and packing material choices from the droplet scale through the process scale.
- Fundamental understanding of how to **optimize absorber design/operation for arbitrary solvents and capture targets**.

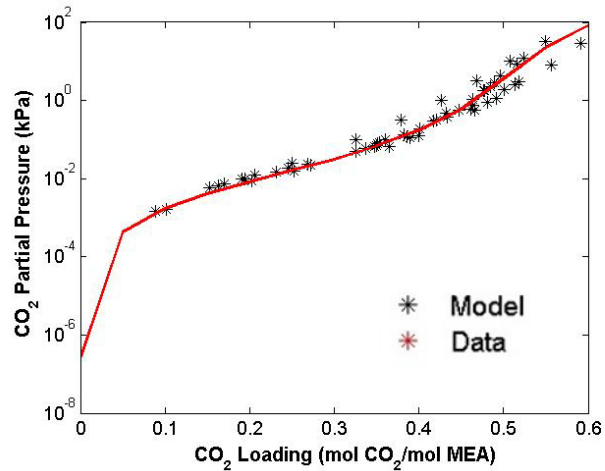
Solvent Model Validation Hierarchy Workflow



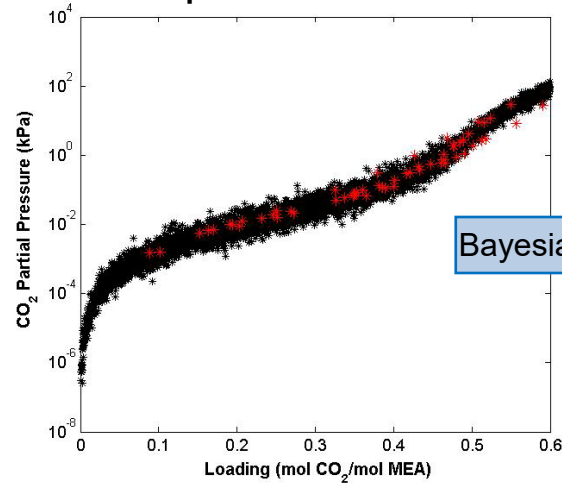
# Uncertainty Quantification Bayesian Inference Example: VLE Models

## VLE Data/Model Comparison at 40°C

Deterministic sub-model

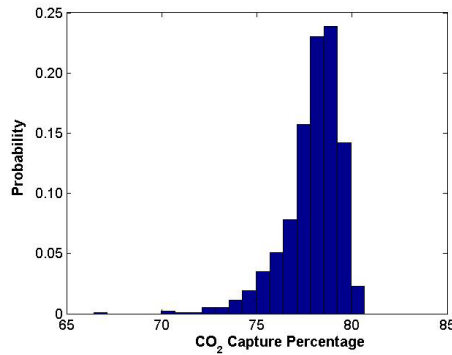
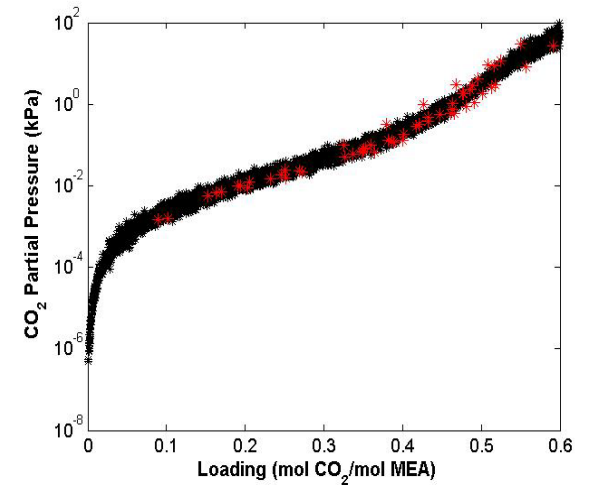


Using best initial guess of parameter set



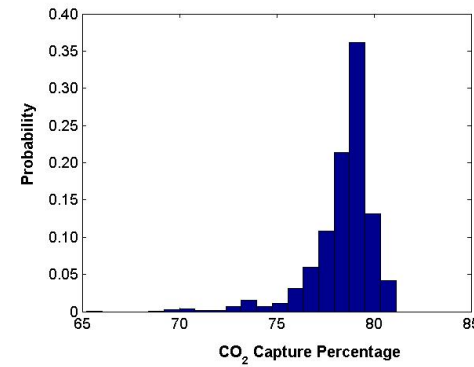
Bayesian inference

Refined parameter set



high uncertainty

Process Model

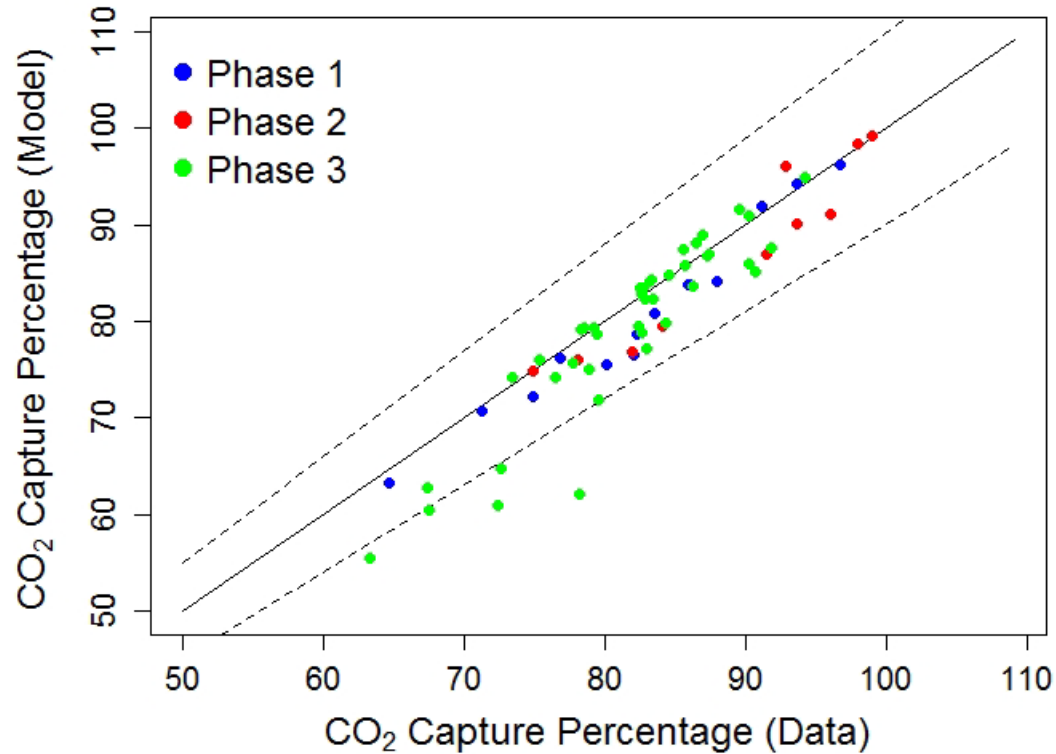


reduced uncertainty

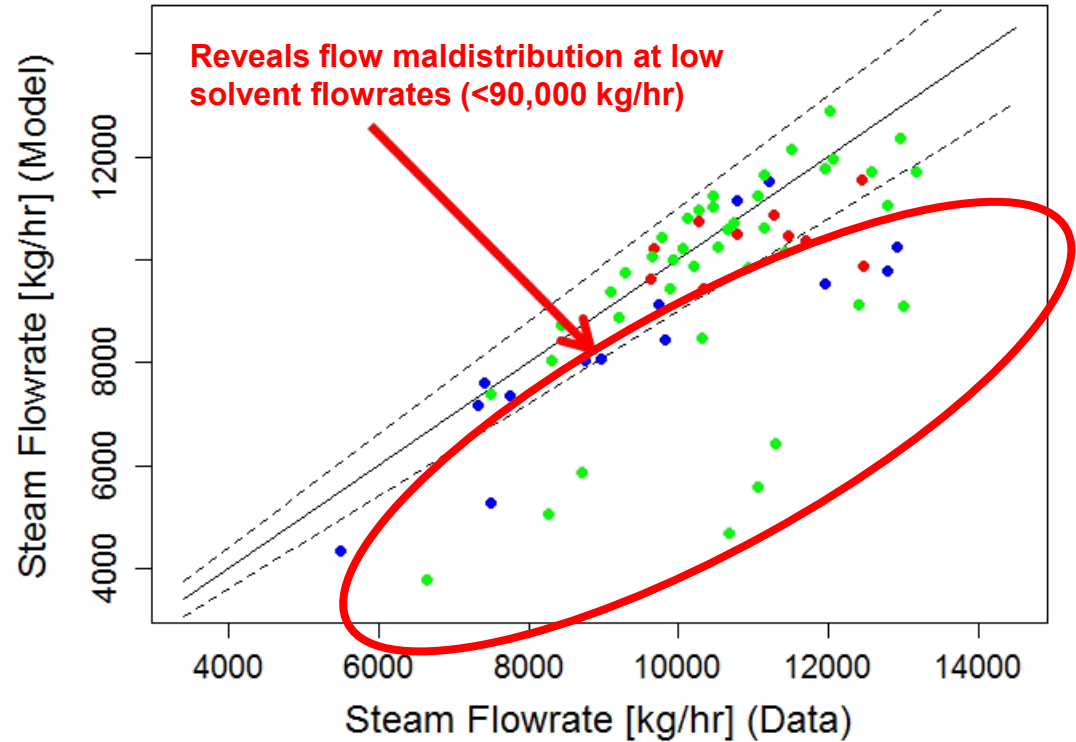
Process Model

# Model Based Insight into Operational Non-Idealities

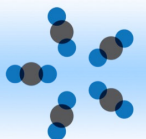
## TCM Absorber Performance\*



## TCM Stripper Performance\*



## Fundamental Model Insight into Data Aberrations





# SDoE Executive Summary

- **First-principles modeling** serves as the foundation for pilot campaign designs
- UQ can be used to **identify data gaps and their effect on key metrics**
- SDoE leverages UQ to more **efficiently inform data collection**
  - Improves MEA CO<sub>2</sub> capture rate prediction by ~60%
- Improved models support **better optimizations**
- Optimization under more refined uncertainty leads to more **robust designs**
- Modeling insights can be used to **guide future R&D decisions** more efficiently

# Deterministic Solvent Modeling Framework

## Vapor-Liquid Equilibrium

$$\hat{f}_i^V = \hat{f}_i^L \longrightarrow \hat{\phi}_i y_i P = \gamma_i^* x_i H_i \quad (\text{for solutes})$$

## Activity Coefficient

$$\ln(\gamma_i) = \frac{1}{RT} \left. \frac{\partial(nG^{ex})}{\partial n_i} \right|_{T,P,n_{j \neq i}} \quad \gamma_i^* = \frac{\gamma_i}{\lim_{x_i \rightarrow 0} \gamma_i}$$

## Reaction Equilibrium Constant

$$\Delta G_{rxn} = -RT \ln(K)$$

## Enthalpy Equations

### Excess Enthalpy

$$H^{ex} = -RT^2 \sum_i x_i \left( \frac{\partial \ln \gamma_i}{\partial T} \right) \Big|_{P,x}$$

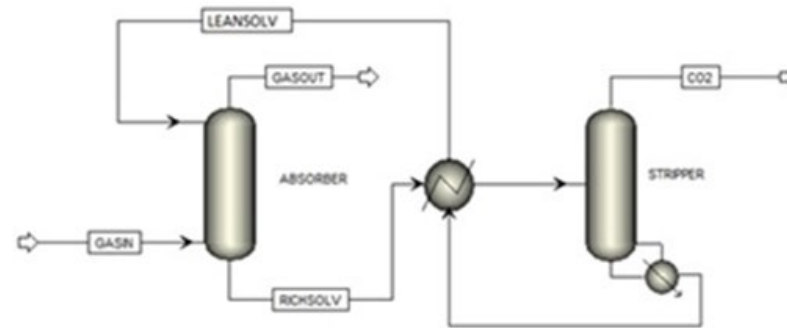
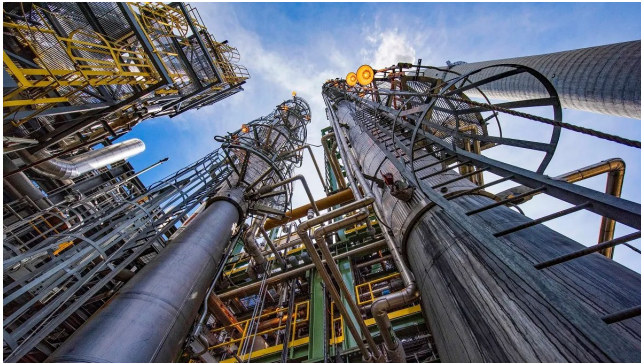
### Heat Capacity

$$H_m^l(T + \Delta T) - H_m^l(T) = \int_T^{T+\Delta T} C_{p,m}^l dT$$

### Heat of Absorption

$$\Delta H_{abs} = \frac{n_{final} H_{final} - n_{initial} H_{initial} - n_{CO_2} H_{CO_2}}{n_{CO_2}}$$

# Deterministic Solvent Modeling Framework



- Validated for National Carbon Capture Center (NCCC) (MEA solvent)
- Validated for Technology Centre Mongstad (TCM) (MEA solvent)

# Novel Solvent-Specific Uncertainty Quantification

## Activity Coefficients

$$\ln \gamma_i = \frac{\sum_j X_j G_{j,i} \tau_{j,i}}{\sum_k X_k G_{k,i}} + \sum_j \frac{G_{i,j} X_j}{\sum_k G_{k,j} X_k} \cdot \left( \tau_{i,j} - \frac{\sum_m X_m G_{m,j} \tau_{m,j}}{\sum_k X_k G_{k,j}} \right)$$

$$\ln H_{ia} = A_{ia} + \frac{B_{ia}}{T}$$

$$\tau_{i,j} = A_{i,j} + \frac{B_{i,j}}{T}$$

$$\ln P_i^{vap} = A_i + \frac{B_i}{T + C_i}$$

$$G_{i,j} = e^{(-\alpha_{i,j} \tau_{i,j})}$$

## Mass Transfer

$$k_G = D_G C_G \left( \frac{a}{d_H} \right)^{0.5} Sc_G^{0.333} Re_G^{0.75} \sqrt{\frac{1}{\varepsilon - h_L}}$$

## Viscosity

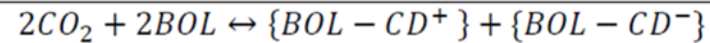
$$\ln \mu_{BOLS} = A_{BOLS} + \frac{B_{BOLS}}{T} + C_{BOLS} \cdot \ln T$$

$$w_{H2O} = \frac{\alpha_{H2O} \cdot MW_{H2O}}{\alpha_{H2O} \cdot MW_{H2O} + MW_{BOL}}$$

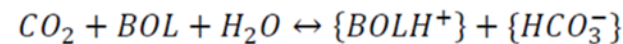
$$\mu_{BOLS-H2O} = \mu_{BOLS} \cdot (1 - w_{H2O}) + \mu_{H2O} \cdot w_{H2O} + D_{Binary} \cdot w_{H2O} \cdot (1 - w_{H2O})$$

$$\mu_{BOLS-CO2-H2O} = \mu_{BOLS-H2O} \cdot e^{\alpha_{CO2} \cdot E_{CO2}}$$

## Kinetics

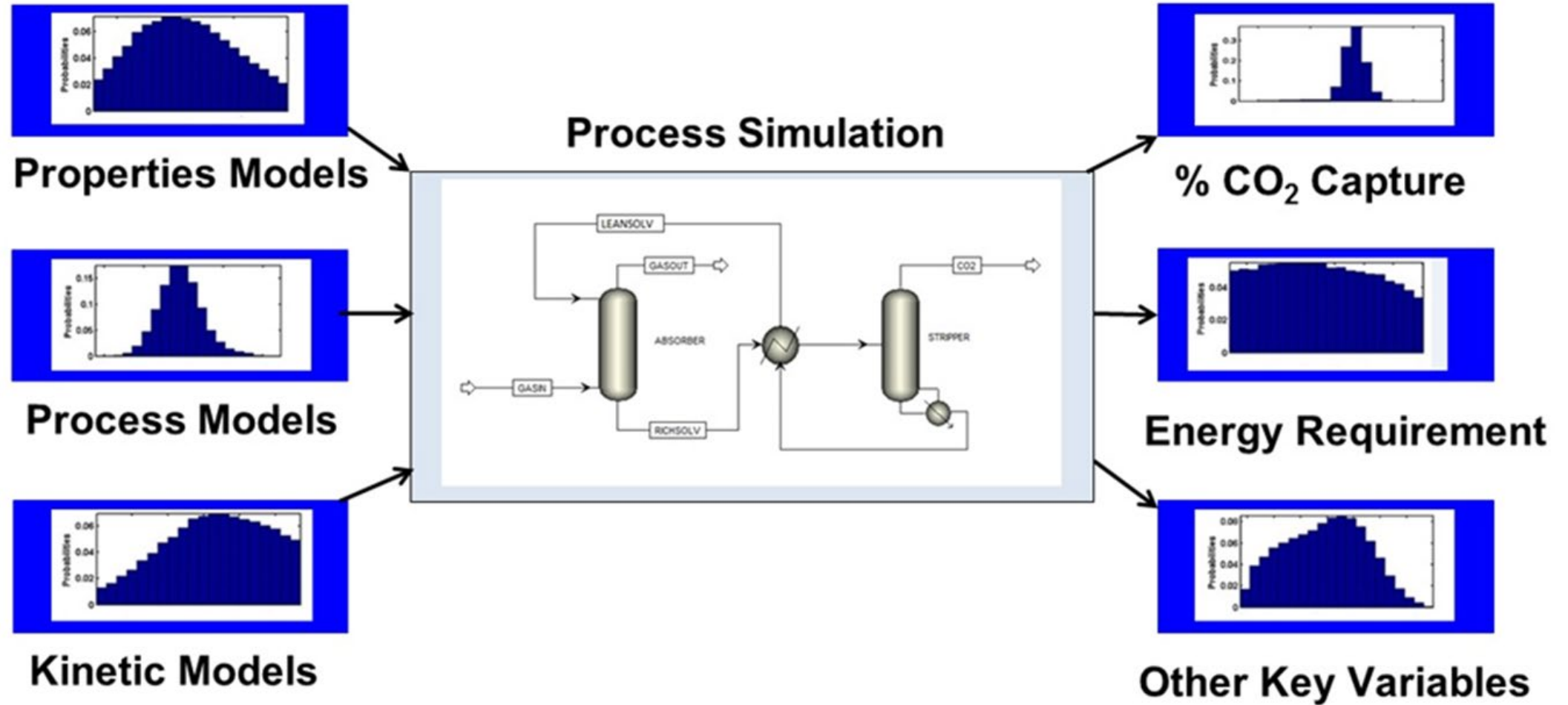


$$r_1 = k_1 \exp\left(-\frac{E_1}{R} \left(\frac{1}{T} - \frac{1}{T_{ref}}\right)\right) a_{CO_2} a_{BOL} \left(1 - \frac{a_{BOL-CD^+} a_{BOL-CD^-}}{(a_{CO_2} a_{BOL})^2 K_1}\right)$$



$$r_2 = k_2 \exp\left(-\frac{E_2}{R} \left(\frac{1}{T} - \frac{1}{T_{ref}}\right)\right) a_{CO_2} a_{BOL} a_{H_2O} \left(1 - \frac{a_{BOLH^+} a_{HCO_3^-}}{K_2}\right)$$

# Novel Solvent-Specific Uncertainty Quantification



# Bayesian Inference

- **Bayesian Inference** provides a framework for updating beliefs of model parameters characterized by epistemic uncertainty in light of collection of new data

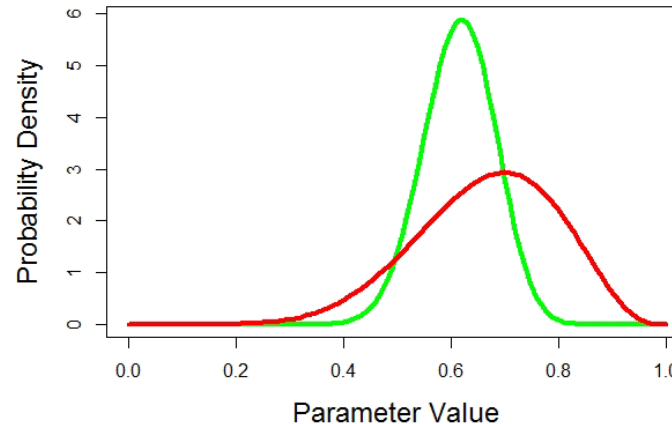
$$\pi(\theta|Z) \propto P(\theta) * L(Z|\theta)$$

Posterior      Prior      Likelihood

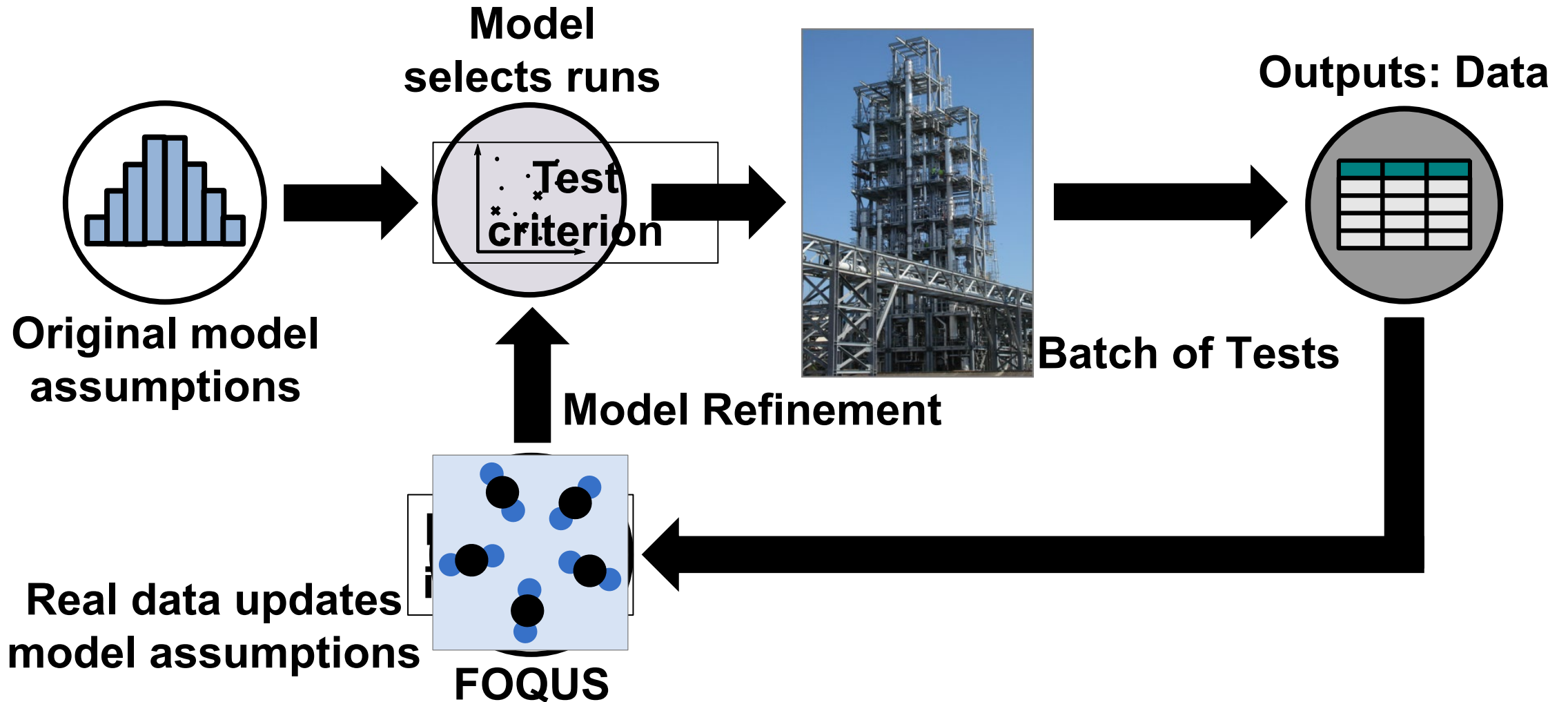
Typical likelihood function (represents discrepancy between model predictions and data values of the output):

$$L(Z|\theta) = \exp\left(-0.5 \sum_{i=1}^M \frac{[F^*(x_i, \theta) - Z(x_i)]^2}{M\sigma_i^2}\right)$$

Representation of Prior and Posterior Distributions (reduction in uncertainty through data collection):

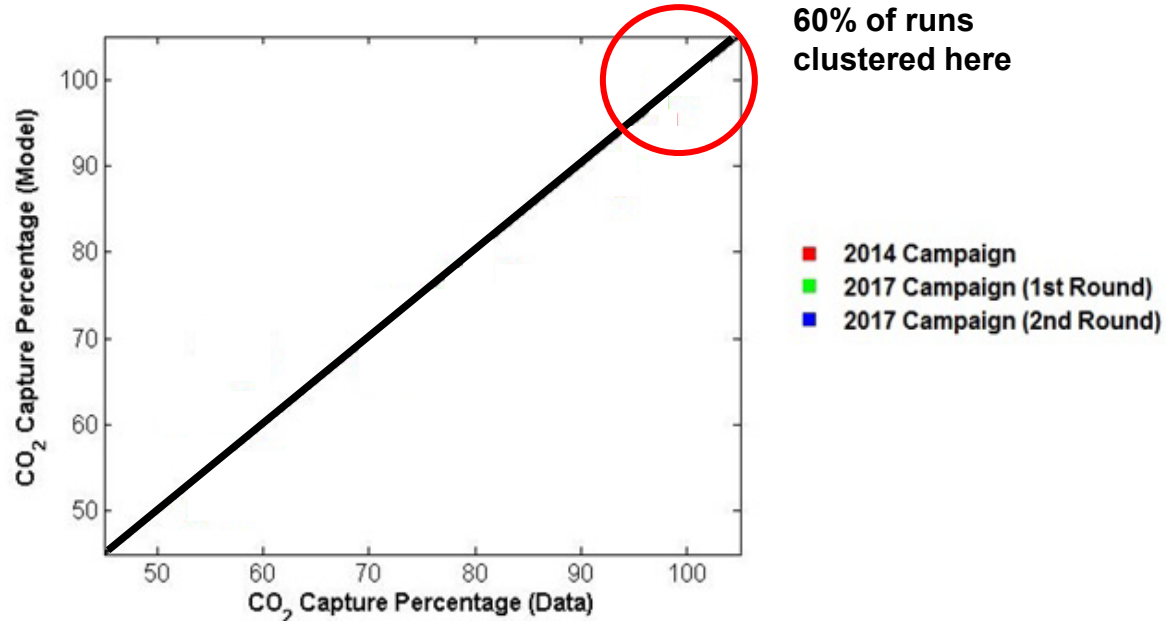


# Sequential Design of Experiments Leverages Real Time Data Generation for Optimal Batch Generation



# NCCC Model Improvement with SDoE Implementation

Three Beds with Intercooling Cases



## 2014 Campaign (Before SDoE)

- Conventional test plan caused “clustering”
- Not ideal for complete understanding
- Used data to refine model



Wait 3 years....

## 2017 Campaign (Using SDoE)

- Much more distributed output
- Much more complete understanding
- *In manner of weeks*, further reduced uncertainty in capture rate by 60%

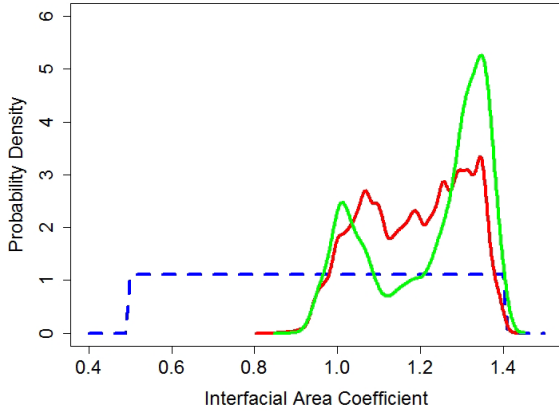


# TCM Model Improvement with SDoE Implementation

## Update in Parameter Distributions for Absorber Packing

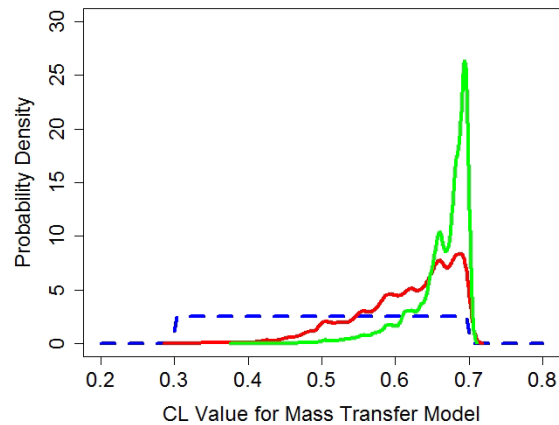


## Reduction in CO<sub>2</sub> Capture Percentage Prediction Accuracy

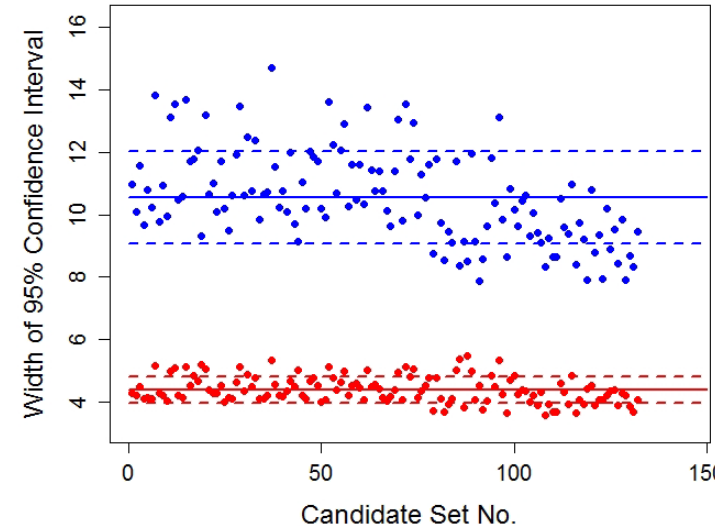


Mass transfer and interfacial area parameters are packing-dependent, and therefore are assigned uniform prior distributions over wide ranges, indicating assumption of relatively large uncertainty before collection of process data.

Bayesian inference, through process data collected using SDoE, results in refined estimates of parameters, and thus reduction in uncertainty in process model and risk associated with scale-up



- — Prior
- — Posterior 1
- — Posterior 2



**Prior CI Width:**  
 $(10.5 \pm 1.5)\%$

**Posterior CI Width:**  
 $(4.4 \pm 0.4)\%$

**Average reduction in uncertainty:**  $58.0 \pm 4.7\%$

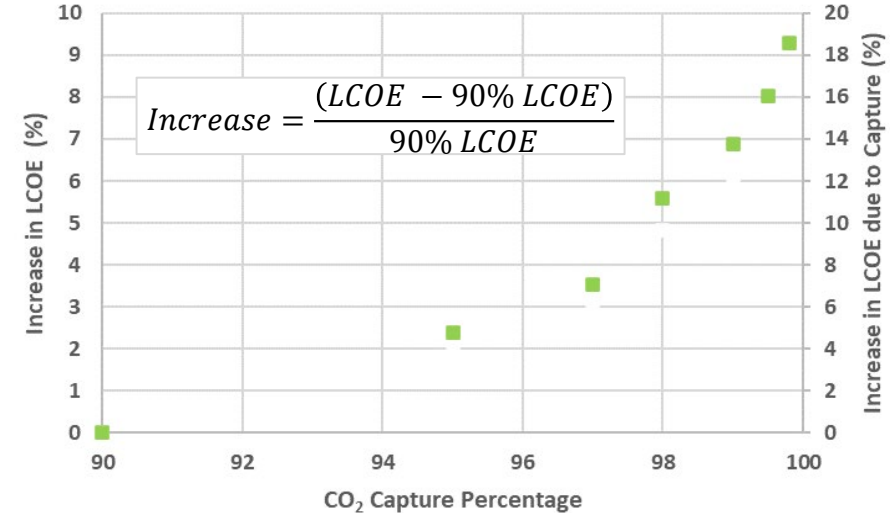
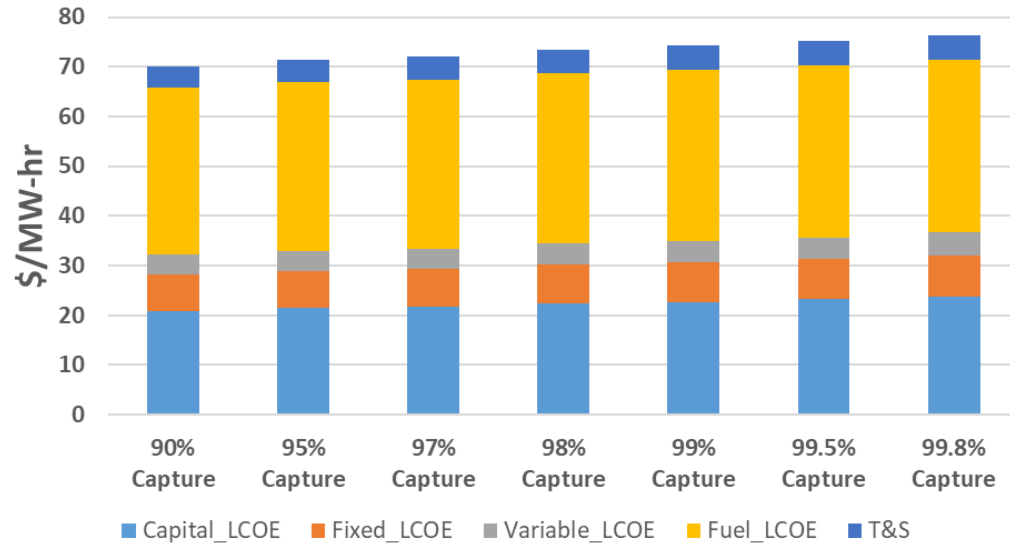
### Candidate set includes variation in:

- Solvent Circulation Rate
- Flue Gas flowrate and CO<sub>2</sub> concentration
- Reboiler steam flowrate

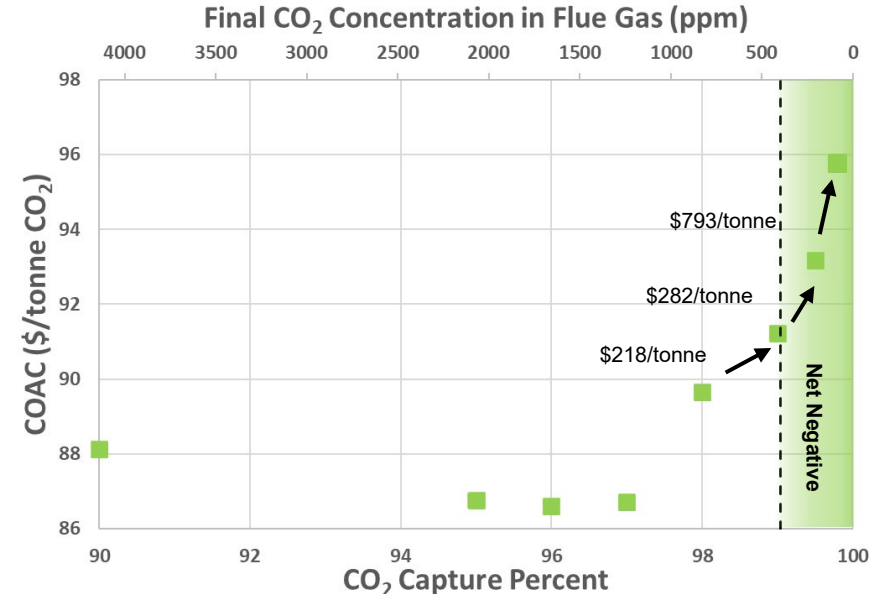
# High Capture Rates with MEA Solvent - NGCC

\*More Detail in Poster by Ben Omell

LCOE Breakdown

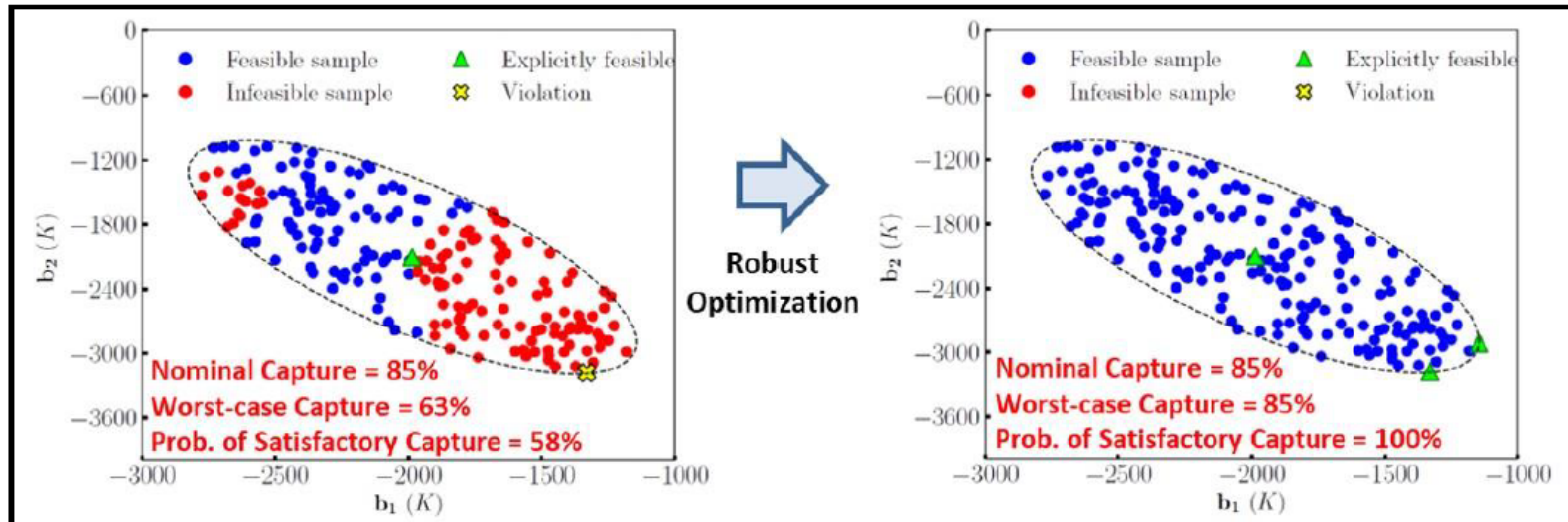


- **LCOE increases linearly from 90→98%**, relatively constant cost of avoided CO<sub>2</sub>.
- Incremental **cost of avoided CO<sub>2</sub> significantly increases** in 98→99.8% capture range.
- Practical considerations (e.g., **need for aux boiler, flexible operation**) will increase LCOE further at high capture percentages





# PyROS: a Pyomo Robust Optimization Solver

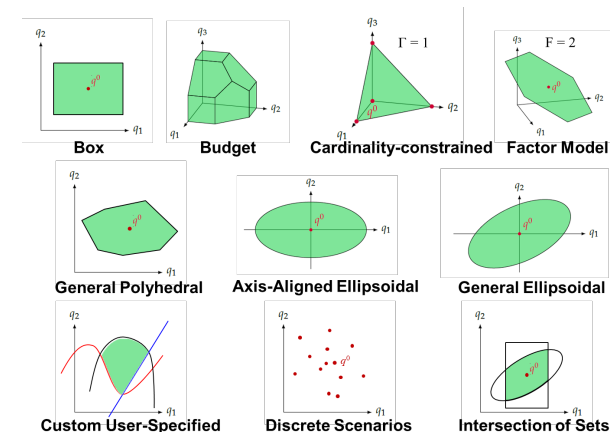


Designs optimized deterministically can easily become infeasible with moderate uncertainty

Robust optimized designs can ensure safety and performance constraints are met amidst anticipated uncertainty

Price of robustness can be quantified, minimized

\*More Detail in Poster by Jason Sherman



Evolution of costs for increasingly robust designs

