

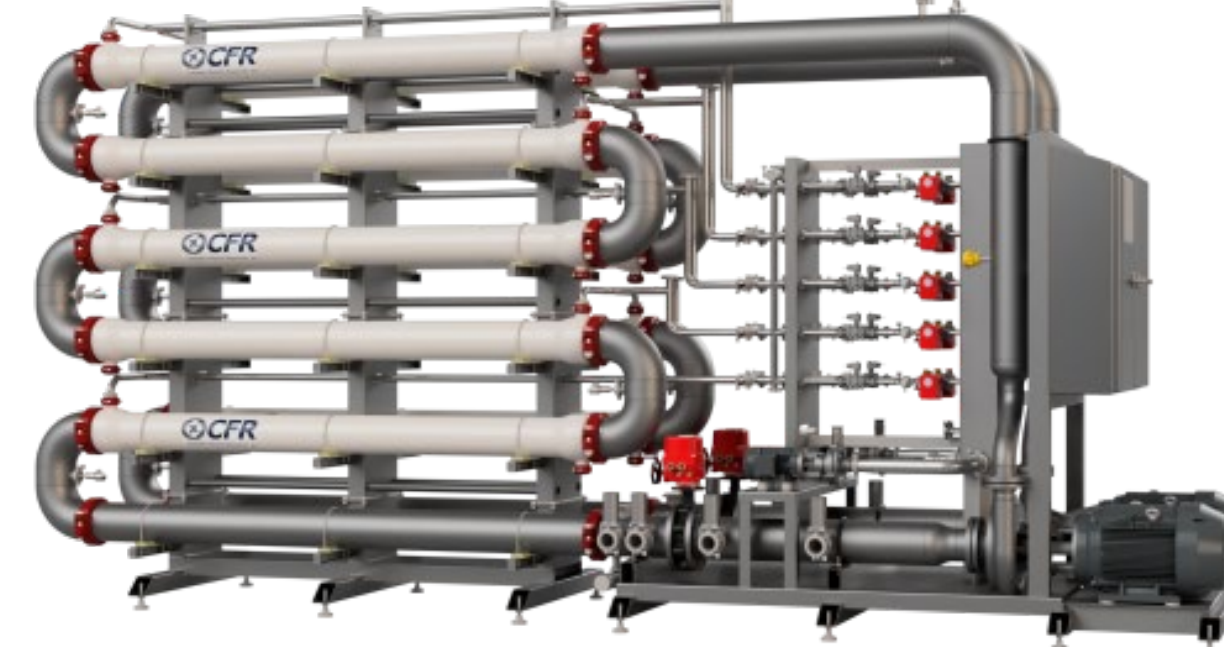
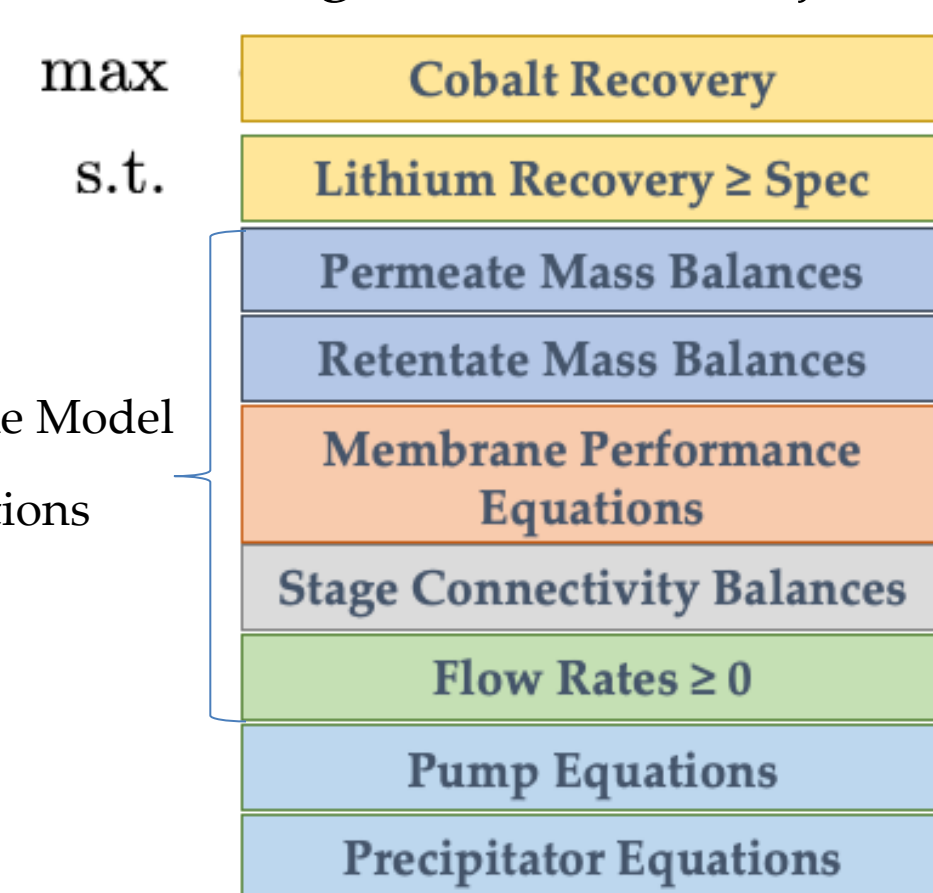


## Diafiltration System Modeling

Membrane technologies are promising low-energy, aqueous processes for critical mineral recovery.

(Interchangeable Li/Co Objectives)

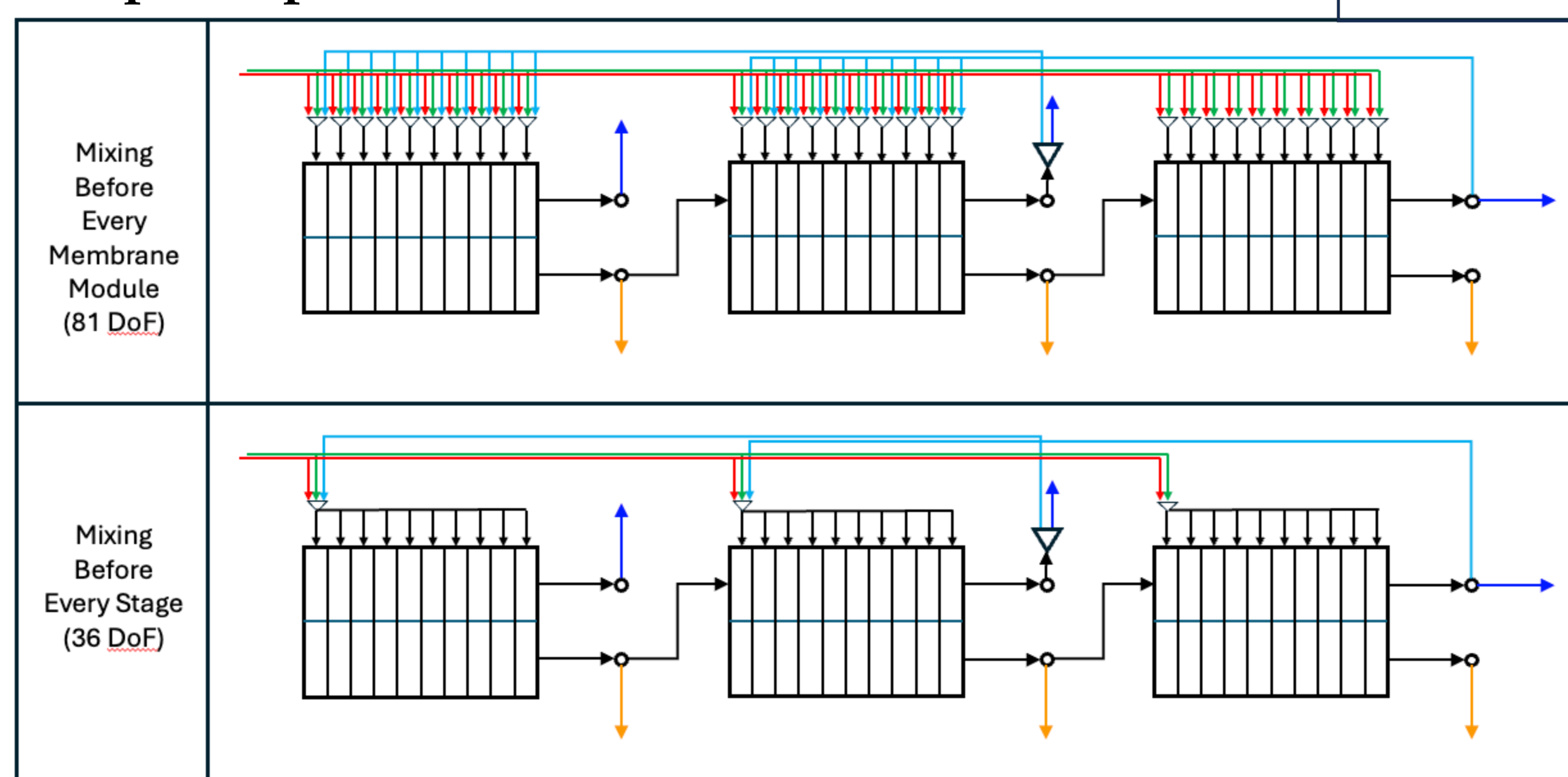
Example Membrane Stage [1]



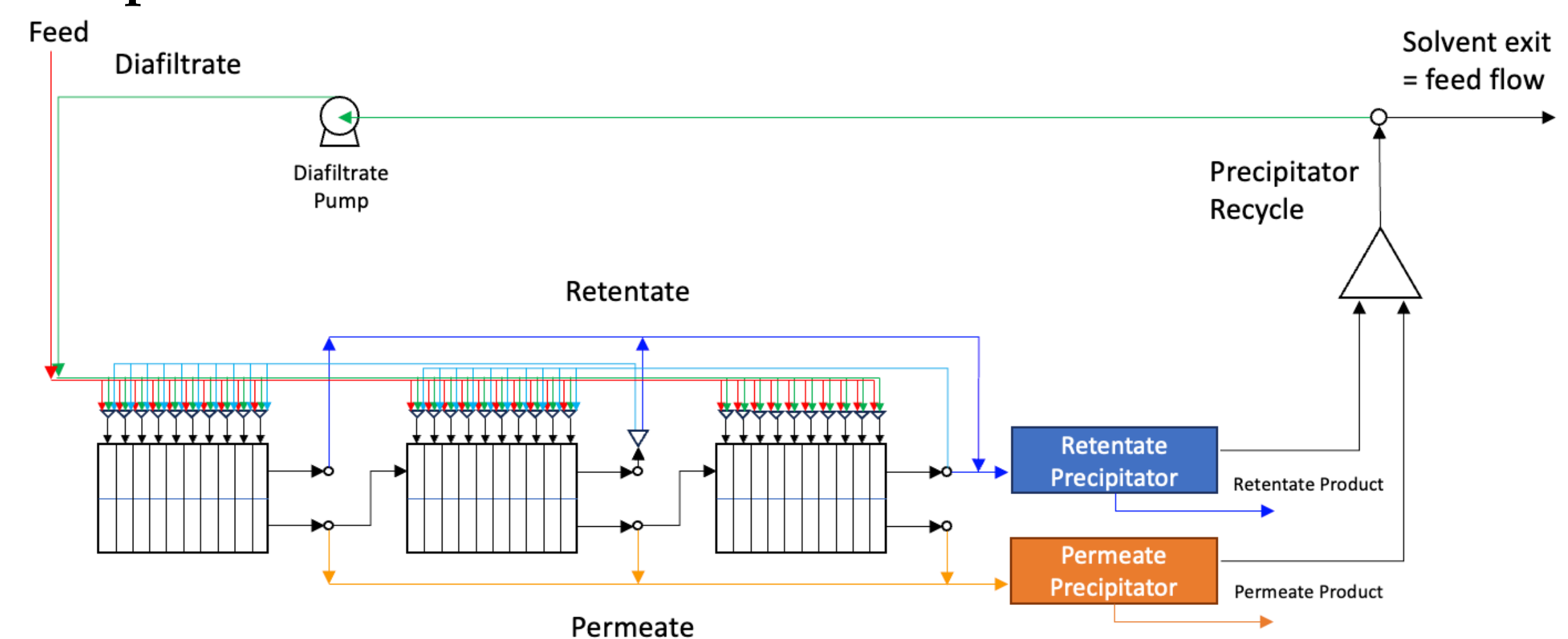
(Based on literature model from [2])



## Example Superstructures:



## Example Flowsheet:



## Robust Optimization Methods

Membrane processes must be able to perform satisfactorily in light of model uncertainties.

- Membrane performance parameters may have manufacturing variability
- Process inlet stream conditions may be different than expected

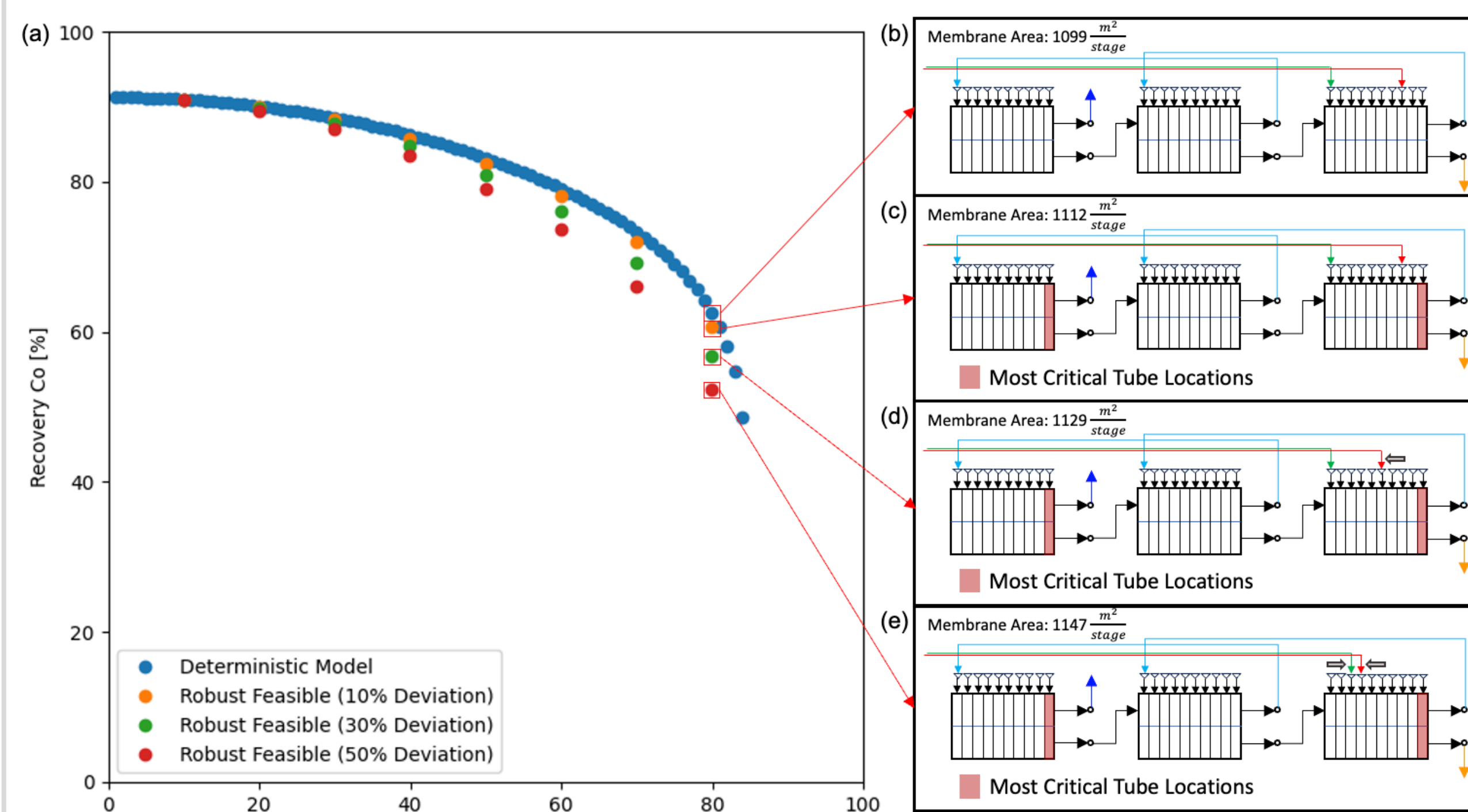
### Design & Control Degrees-of-Freedom:

- Membrane area is set during process construction
- Inlet flow rates and locations are adjustable during operation

**Pyomo Robust Optimization Solver (PyROS)** can obtain robust optimal solutions that are feasible for all realizations of uncertainty<sup>[3,4]</sup>

## Uncertainty in Membrane Performance

Manufacturing variability in membrane sieving may reduce process performance. Robust designs can satisfy recovery requirements under these conditions.



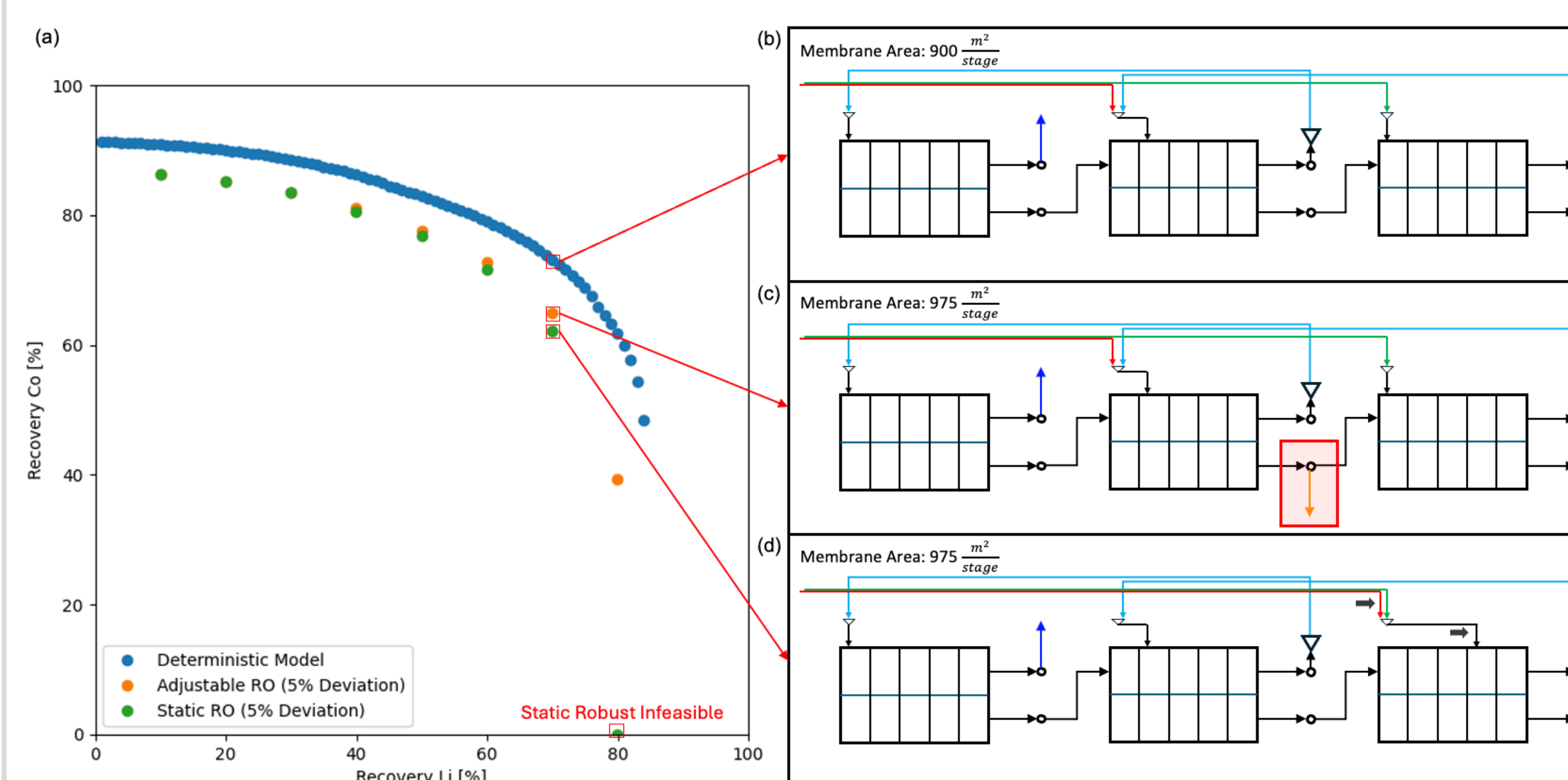
- As a "cost of robustness", robust optimization with larger uncertainty sets results in worse objectives relative to deterministic solutions

### Insights:

- Increasing membrane area helps to proactively maintain lithium recovery
- In the worst-case scenario, membrane tube modules right before product streams have high cobalt sieving.
  - These locations have the highest concentration of solutes and are more vulnerable to loss of product.

## Uncertainty in Process Inlet Stream

Uncertainty in the feed flow and quality of raw materials make membrane process design difficult. Adjustable robust optimization takes into account built-in process flexibility and can potentially find better process designs.



- Static robust optimization assumes all decisions are made during process construction. Adjustable robust optimization assumes some decisions as recourse to react to uncertain scenarios.

### Insights:

- A more flexible process can sustain satisfactory process performance under conditions where static designs fail.
- Alternative lithium product streams can maintain lithium recoveries with potentially higher cobalt recoveries.

## Diafiltration System Costing

Optimization of a costing objective can determine optimal diafiltrate flow rate and yield cost effective designs.

$$\min OPEX + \epsilon CAPEX$$

$$\text{s.t. } OPEX = RR_{mem} c_{mem} A_{mem} + c_{pump}^{operate} \frac{Q_{dia}}{Q_{pump}}$$

$$CAPEX = c_{mem} A_{mem} + c_{pump}^{install} \frac{Q_{dia}}{Q_{pump}}$$

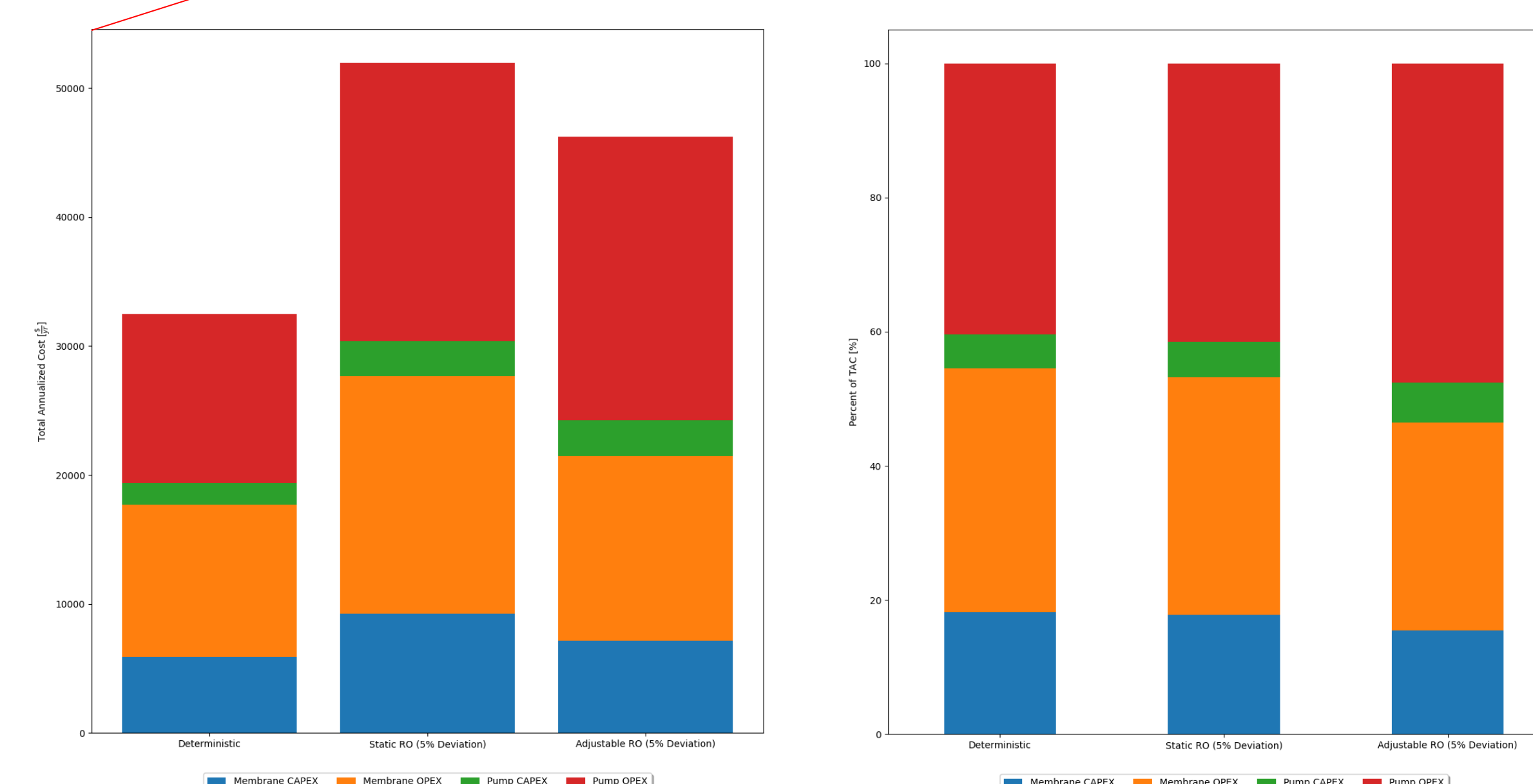
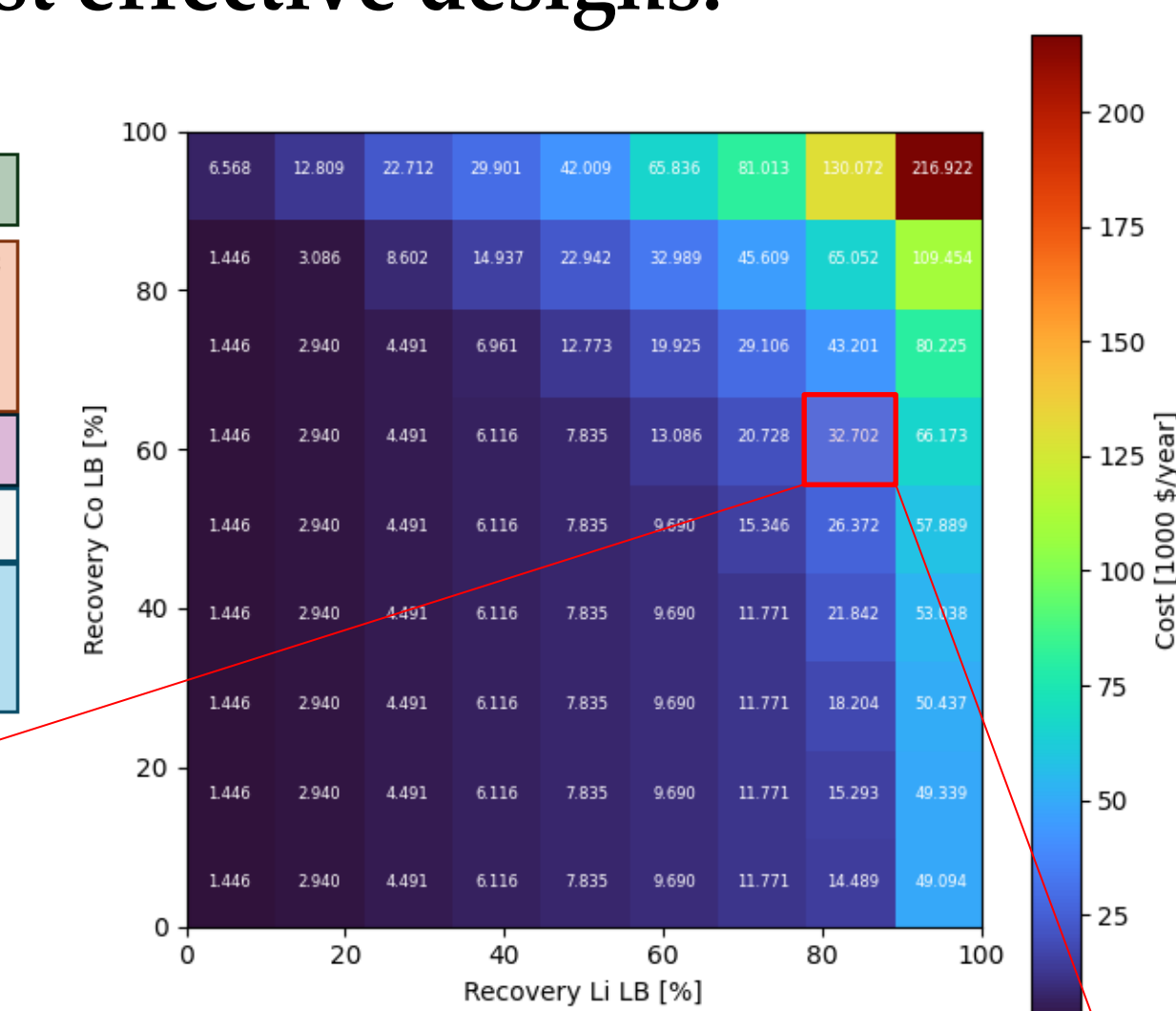
$$Recovery_s \geq Spec_s \quad \forall s \in \{Li, Co\}$$

Membrane Model Equations

Pump Equations

Precipitator Equations

(Costing parameter data from [5-7])



- Insights from previous case studies still apply with costing model
- A cost optimal diafiltrate flow balances the cost of increasing flow rate with benefit of improving membrane system performance and flexibility

## Conclusions and Future Work

### Conclusions:

- We applied robust optimization methodologies on a Co/Li diafiltration flowsheet to generate optimal designs immune to membrane manufacturing variability and uncertain process feed flow and concentrations.
- Based on a simple costing model, we showed how robust designs can maintain performance requirements at a slightly higher cost compared to their deterministic counterparts.

### Future work:

- Apply robust optimization on multiperiod membrane models to investigate uncertainty in time-varying raw material inlets and fouling over time.
- Obtain robust designs using PrOMMiS's high-fidelity costing model.
- Explore applications with other critical minerals.

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